

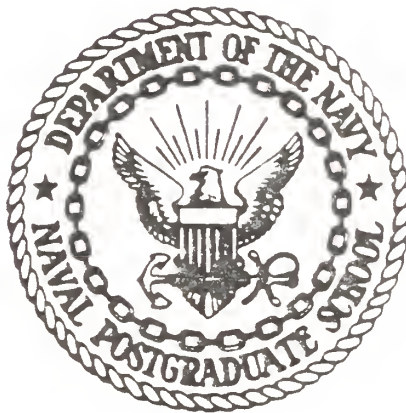
THE FINITE ELEMENT METHOD APPLIED TO  
FLOWS IN TURBOMACHINES

Valentin Francisco Gavito

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## Monterey, California



# THESIS

THE FINITE ELEMENT METHOD APPLIED TO FLOWS IN  
TURBOMACHINES

by

Valentin Francisco Gavito, Jr.

December 1976

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TURBOMACHINES

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requirements for the degree of

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# ABSTRACT

The finite element method is applied to the two-dimensional, inviscid, compressible radial equilibrium equation for axial compressors. Isoparametric elements are used along with three-point Gaussian integration for stiffness matrix evaluation. The radial equilibrium equation is put into quasi-harmonic form for stream function formulation and results are presented using an isentropic flow assumption. Axial velocity profiles at rotor and stator blade edges are compared with published performance data of the NASA Task-1 stage transonic compressor and with numerical finite element results of Hirsch and Warzee.



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## I. INTRODUCTION

### A. PROBLEM STATEMENT AND OBJECTIVE

The prediction of meridional flows within turbomachines, be they compressors or turbines, is a difficult but important part of the design process. The difficulty arises from the presence of three-dimensional and viscous effects within all turbomachines and the importance arises from the necessity to design accurately and efficiently.

To simplify the problem of viscous, three-dimensional analysis, Wu [Ref.1] showed that this complicated flow may be analyzed by solving two interrelated flows: one being the blade-to-blade flow describing the flow between rotating blades and the other being the meridional through flow which describes the radial equilibrium. These flows are depicted in Fig 1. In addition, an inviscid and axi symmetric assumption is made in the through-flow thereby simplifying the flow to a two-dimensional, axi symmetric, inviscid, and compressible analysis.

Three methods may be found in current reports regarding the solution of the radial equilibrium equation. The first two are the streamline curvature method [Ref.2,3,and 4] and the matrix method [Ref.5 and 6] which is basically a finite difference technique. The third, a relatively new method, is the finite element method. As shown by Hirsch and Warzee [Ref.7]', the solution of the radial equilibrium equation by the finite element method is achieved by arranging the



equation for the stream function in quasi-harmonic form.

Due to the excellent results reported in Ref.7 and to further the research effort for finite element techniques in fluid flow problems, the purpose of this thesis is two fold. Firstly, the goal was to formulate a computer program for solution of the radial equilibrium equation paralleling the steps as presented by Hirsch and Warzee. Secondly, after suitable verification of computer results with those of Hirsch and Warzee, the goal was to compare computer predicted flows with measured performance data of the Naval Post Graduate School's transonic compressor.

The purpose of this paper is to present a report on the results obtained thus far. In Section II, the derivation of the radial equilibrium equation is presented followed by the application of the finite element method to this equation. Section III describes the computer program in some detail. Section IV contains selected test cases which were used in program testing and checking. In Section V, conclusions are presented along with recommendations for further study and work on the project. The appendices contain the program listing along with a sample test case for reference by the user. In addition, a list of references is contained for further reading on the subject of this paper.



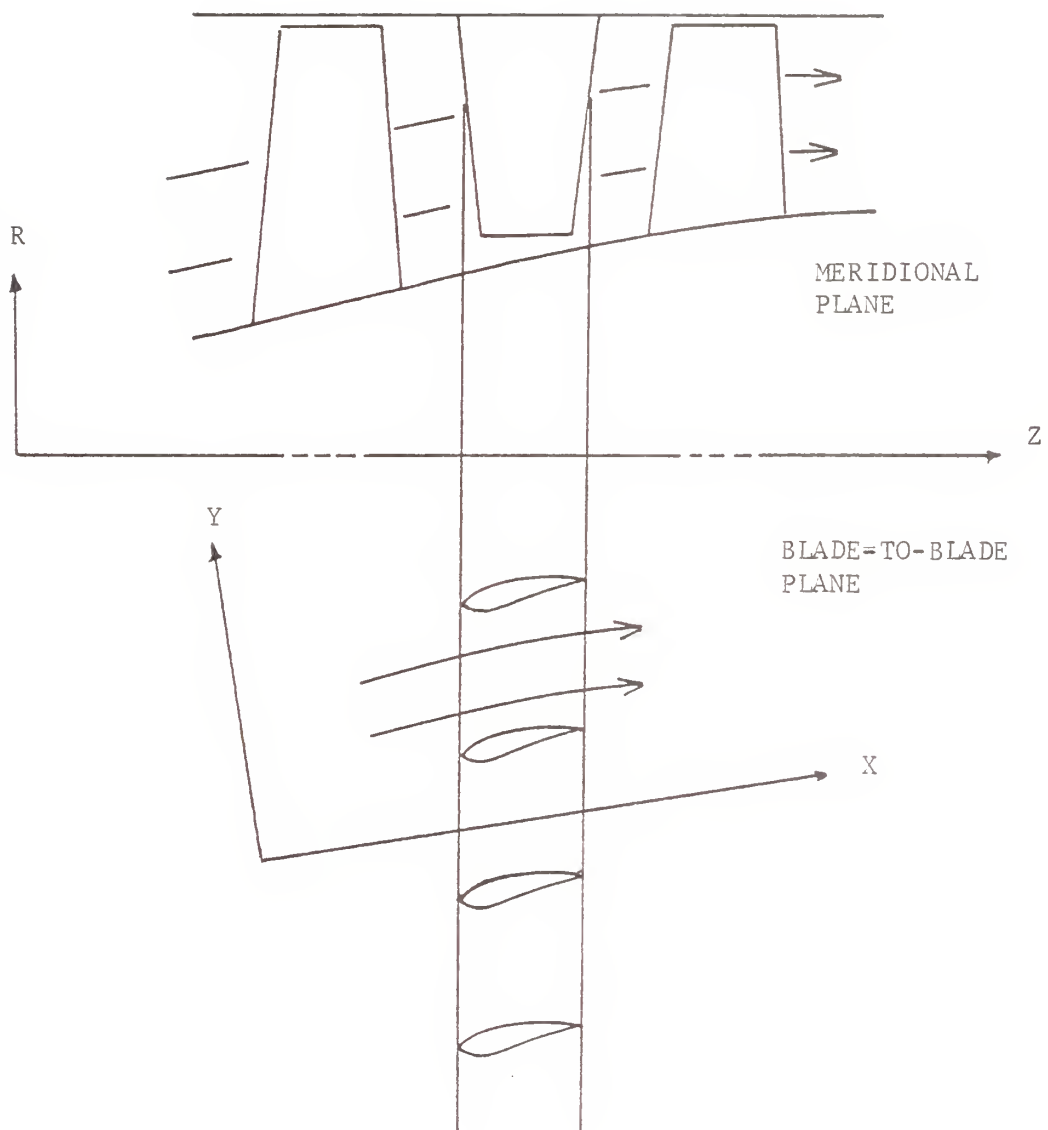


Figure 1 - MERIDIONAL AND BLADE-TO-BLADE PLANES



## II. THEORY

### A. THE DERIVATION OF THE RADIAL EQUILIBRIUM EQUATION

The following discussion is taken from Ref. 7 with slight changes in notation. The basic turbomachine geometry to be analyzed is depicted in Fig 2. Although the machine noted is one stage of a compressor, a similar analysis to the one that follows may be applied to other machines such as axial turbines and mixed-flow machines.

One begins with the Euler equation assuming the viscous forces to be negligible.

$$\frac{d\vec{V}}{dt} + (\vec{V} \cdot \nabla) \vec{V} = \nabla P / \rho \quad (\text{II.A.1})$$

The continuity equation, assuming unsteady flow is,

$$\frac{d\rho}{dt} + \nabla(\rho \vec{V}) = 0 \quad (\text{II.A.2})$$

The First Law of thermodynamics in a fluid field becomes,

$$T \nabla s = \nabla h - \nabla P / \rho \quad (\text{II.A.3})$$





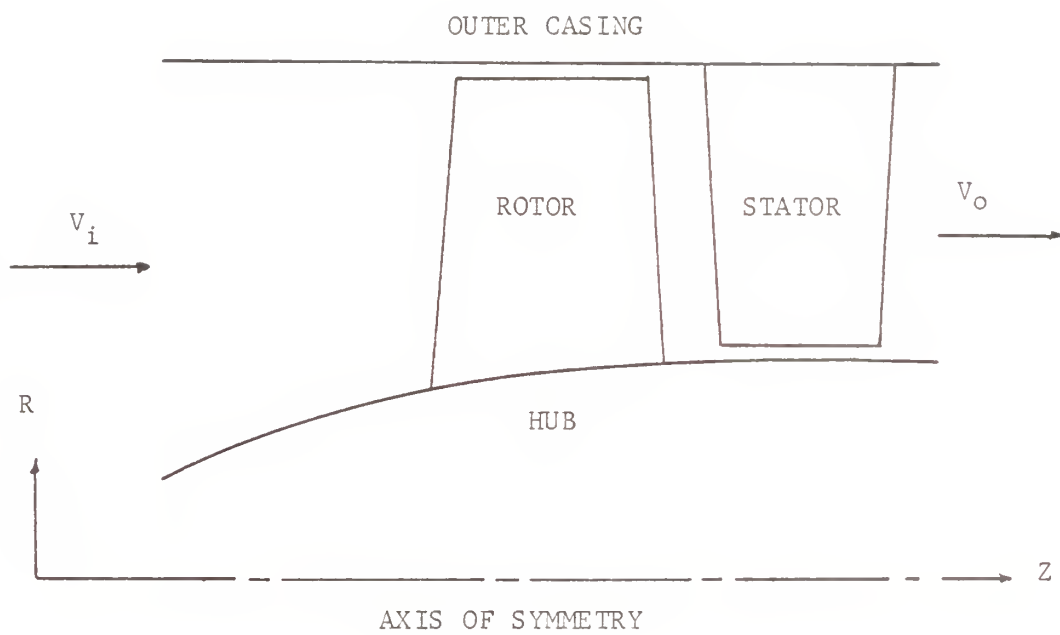


Figure 2 - TURBOMACHINE GEOMETRY



Substituting equation (II.A.3) into equation (II.A.1) leads to the Crocco equation,

$$\frac{d\vec{V}}{dt} - \vec{V} \times (\nabla \times \vec{V}) = T \nabla S - \nabla H \quad (\text{II.A.4})$$

where  $H$  is the total enthalpy.

Assuming a steady and adiabatic flow, the energy equation becomes simply,

$$(\vec{V} \cdot \nabla) H = 0 \quad (\text{II.A.5})$$

which shows that along a streamline in a stationary system, the total enthalpy is constant.

In a relative system, such as the case in a rotor blade row, the total relative velocity,  $\vec{W}$ , can be expressed in the following form,

$$\vec{W} = \vec{V} + \vec{\omega} \times \vec{R} = \vec{V} + \vec{U} \quad (\text{II.A.6})$$

where  $\vec{\omega}$  is the constant angular velocity and  $\vec{U}$  is the constant peripheral speed of the relative system.

Now, the Crocco equation in a relative system becomes,

$$\frac{d\vec{W}}{dt} - \vec{W} \times (\nabla \times \vec{W}) = T \nabla S - \nabla \left( h + \frac{W^2}{2} - \frac{\omega^2 R^2}{2} \right) \quad (\text{II.A.7})$$

Parallel to equation (II.A.5) for the stationary system, the energy equation, assuming steady and adiabatic (relative) flow in a relative system, becomes



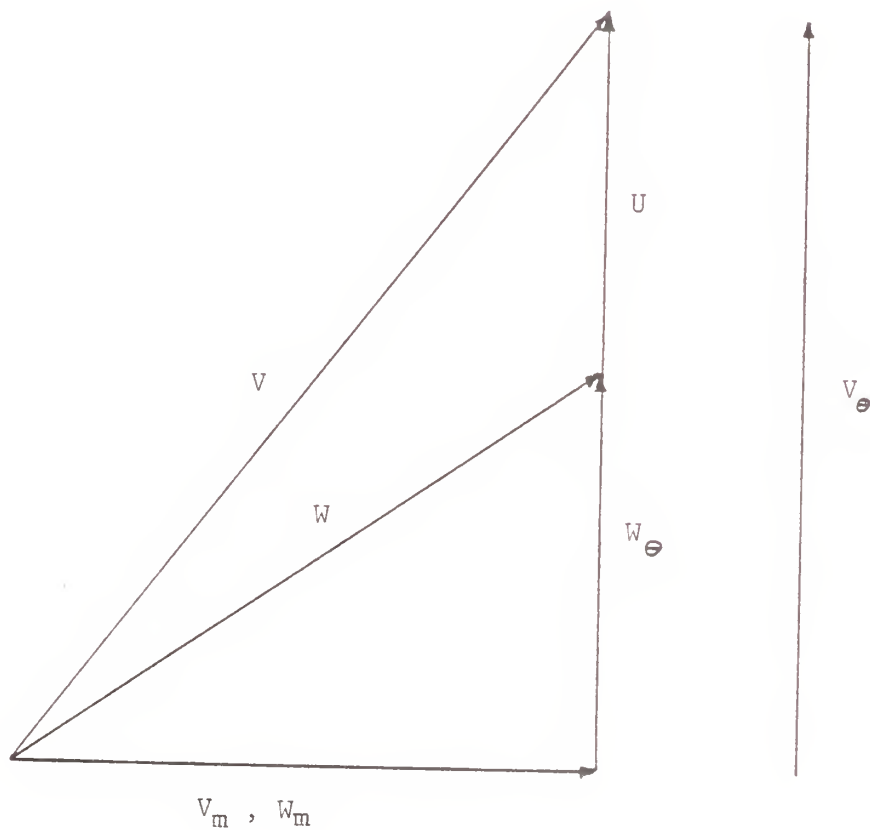
(II.A.8)

$$(\vec{W} \cdot \nabla) H_R = 0$$

where  $H_R$  is the relative total enthalpy expressed as follows,

$$H_R = h + \frac{W^2}{2} - \frac{\omega^2 R^2}{2} \quad (\text{II.A.9})$$

From the following velocity diagram,





equation (II.A.9) may be arranged as follows.

Since,

$$W_m^2 + W_\theta^2 = W^2 = V_m^2 + (V_\theta - u)^2 \quad (\text{II.A.10})$$

then,

$$W^2 = V_m^2 + V_\theta^2 - 2uV_\theta + u^2 \quad (\text{II.A.11})$$

and,

$$W^2 = V^2 + u^2 - 2uV_\theta \quad (\text{II.A.12})$$

Substituting equation (II.A.12) into equation (II.A.9) leads to the following relation,

$$H_R = h + \frac{V^2}{2} - uV_\theta = H - uV_\theta \quad (\text{II.A.13})$$

Equation (II.A.8) shows that  $H_R$  is constant along a streamline in a relative system.

Upon integrating equation (II.A.8) between the rotor inlet and outlet, the Euler equation for turbomachines is found,

$$\Delta H \Big|_{IN}^{OUT} = \Delta (\vec{U} \cdot \vec{V}_\theta) \Big|_{IN}^{OUT} \quad (\text{II.A.14})$$





It may be shown [Ref.9] that by circumferentially averaging equation (II.A.1), and under the axi symmetric flow assumption the following relation is valid,

$$-\vec{V} \times (\nabla \times \vec{V}) = T \cdot \nabla S - \nabla H + F_b + F_d \quad (\text{II.A.15})$$

where  $F_b$  is the body force of the blades acting on the fluid and all variables are mean values along the direction of the circumference. Hence equation (II.A.15) is an approximation for axi symmetric flow. As a final note on equation (II.A.15), since the viscous forces were neglected in equation (II.A.1), there must be a force introducing the entropy variations along the blade. This force is proportional to the pressure loss coefficient and is labeled  $F_d$ , the dissipative force.  $F_d$  produces work which in turn produces entropy production radially along the blade. Under the axi symmetric assumption, entropy varies axially and radially only and is assumed to be proportional to the pressure loss coefficients [Ref. 2 and 8].

Due to boundary conditions imposed on the problem and the axi symmetric assumption, cylindrical coordinates,  $(r, \theta, z)$ , will be used in all subsequent analysis. Therefore, equation (II.A.15), in cylindrical coordinates and with axial symmetry is as follows,

$$\frac{V_\theta}{R} \frac{\partial}{\partial R} (R V_\theta) - V_z \left( \frac{\partial}{\partial z} V_R - \frac{\partial}{\partial R} V_z \right) = \frac{\partial H}{\partial R} - T \frac{\partial S}{\partial R} - F_{br} - F_{dr} \quad (\text{II.A.16})$$

$$\frac{V_z}{R} \frac{\partial}{\partial z} (R V_\theta) + \frac{V_R}{R} \frac{\partial}{\partial R} (R V_\theta) = F_\theta \quad (\text{II.A.17})$$



$$V_R \left( \frac{\partial}{\partial z} V_R - \frac{\partial}{\partial R} V_z \right) - \frac{V_\theta}{R} \frac{\partial}{\partial z} (R V_\theta) = \frac{\partial H}{\partial z} - T \frac{\partial S}{\partial z} - F_z \quad (\text{II.A.18})$$

It is important to note here that under the axisymmetric assumptions, equation (II.A.15) reduces to the following,

$$\vec{V} \cdot \vec{F}_b = 0 \quad (\text{II.A.19})$$

Likewise in a relative system (rotor), the axisymmetric assumption leads to the following,

$$\vec{W} \cdot \vec{F}_b = 0 \quad (\text{II.A.20})$$

Equation (II.A.16) describes the meridional through flow radial equilibrium equation for the finite element method. Since one is concerned with the meridional plane, the following derivative expression is taken from Fig 3.

$$V_m \frac{\partial}{\partial m} = V_R \frac{\partial}{\partial R} + V_z \frac{\partial}{\partial z} \quad (\text{II.A.21})$$

Therefore equation (II.A.17) reduces to,

$$R F_\theta = V_m \frac{\partial}{\partial m} (R V_\theta) \quad (\text{II.A.22})$$

which reveals that in a duct where there are no blades and therefore no blade forces, angular momentum is constant



along a streamline. In that case,

$$\frac{d}{dm}(RV_\theta) = 0 \quad (\text{II.A.23})$$

As shown in Ref.9, the circumferentially averaged continuity equation is the following,

$$\frac{d}{dr}(\rho R b V_r) + \frac{d}{dz}(\rho R b V_z) = 0 \quad (\text{II.A.24})$$

where  $b$  is the blockage factor defined by Hirsch and Warzee as the tangential area reduction due to the thickness of the blade.

$$b = 1 - \frac{t}{s} \quad (\text{II.A.25})$$

where  $t$  is blade thickness and  $s$  is blade spacing.



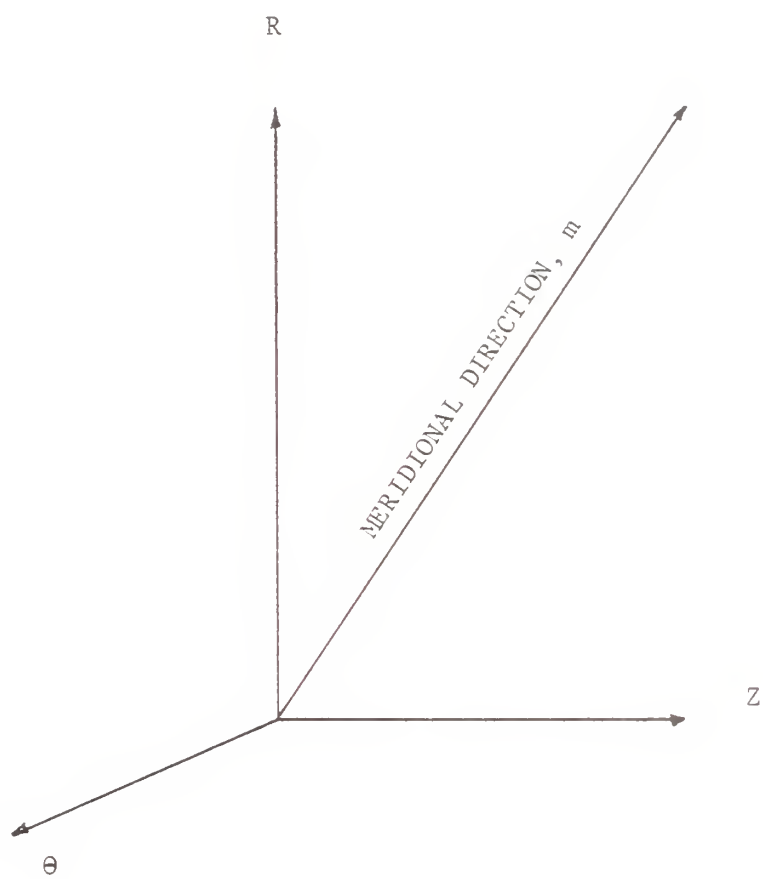


Figure 3 - MERIDIONAL PLANE





One further step in the formulation of the radial equilibrium equation for solution by the finite element method involves introducing the stream function. In cylindrical coordinates, the stream functions are defined as follows,

$$V_z = \frac{1}{rRb} \frac{\partial \psi}{\partial R} \quad (\text{II.A.26})$$

$$V_\theta = - \frac{1}{rRb} \frac{\partial \psi}{\partial z} \quad (\text{II.A.27})$$

Substituting these expressions into equation (II.A.16), the equation becomes,

$$\begin{aligned} \frac{\partial}{\partial R} \left( \frac{1}{rRb} \frac{\partial \psi}{\partial R} \right) + \frac{\partial}{\partial z} \left( \frac{1}{rRb} \frac{\partial \psi}{\partial z} \right) = \frac{1}{V_z} \left[ \frac{\partial H}{\partial R} - T \frac{\partial s}{\partial R} \right. \\ \left. - \frac{V_\theta}{R} \frac{\partial}{\partial R} (RV_\theta) - F_{br} - F_{dr} \right] \end{aligned} \quad (\text{II.A.28})$$

The right hand side of equation (II.A.28) is applicable to the absolute flows in the stator and duct regions. For relative flows such as those in the rotor, the right hand side is modified by replacing the total enthalpy,  $H$ , by the relative total enthalpy,  $H_r$ , and the quantity  $V_\theta/R$  is replaced by  $W_\theta/R$ .

As a last assumption in the formulation of the governing relation for the meridional through flow radial equilibrium equation, both the radial component of the body force,  $F_b$ , and the radial component of the dissipative force,  $F_d$ , are neglected. This assumption, [Ref.1,8] does not hamper the accuracy of the results for conditions at design speed. Even though published compressor performance data used for



the test case in this thesis was obtained at 0.5 design speed, these force terms were also neglected in the computer program. As will be shown later, this assumption could possibly have had adverse effects on the predicted axial velocity profiles at the rotor hub and tip regions.

The final representation of the meridional radial equilibrium equation to be solved by the finite element method is as follows,

$$\frac{\partial}{\partial R} \left( k \frac{\partial \psi}{\partial R} \right) + \frac{\partial}{\partial z} \left( K \frac{\partial \psi}{\partial z} \right) + f = 0 \quad (\text{II.A.29})$$

where,

$$k = \frac{1}{\rho R b} \quad (\text{II.A.30})$$

and

$$f = \frac{1}{V_z} \left[ T \frac{\partial s}{\partial R} - \frac{\partial H}{\partial R} + \frac{V_\theta}{R} \frac{\partial}{\partial R} (R V_\theta) \right] \quad (\text{II.A.31})$$

## B. THE FINITE ELEMENT METHOD APPLIED TO THE RADIAL EQUILIBRIUM EQUATION

In order to formulate equations (II.A.29) through (II.A.31) in matrix form for solution by the finite element method, one must apply a weighted residual technique to the equations for numerical solution. The weighted residual method used here is the Galerkin's Method. The following discussion is taken from Ref. 7 with only slight changes in notation.

Rewriting equation (II.A.29) and dividing through by  $R$ , one has,



(II.B.1)

$$\frac{1}{R} \left\{ \frac{\partial}{\partial R} \left( K \frac{\partial \psi}{\partial R} \right) + \frac{\partial}{\partial z} \left( K \frac{\partial \psi}{\partial z} \right) + f \right\} = 0$$

where this equation represents the flow in the volume, V.

The boundary condition for this partial differential equation, after dividing through by R, is,

$$\frac{1}{R} \left\{ K \frac{\partial \psi}{\partial n} + \alpha_1 (\psi - \psi_0) \right\} = 0 \quad (\text{II.B.2})$$

where this equation solves the flow on the closed boundary of the volume, or, S.

By applying the weighted residual process to equations (II.B.1) and (II.B.2) and using an arbitrary weighting function,  $W(r, z)$ , one has

$$\int_V W(r, z) r_{vol} dV + \int_S W(r, z) r_{sur} dS = 0 \quad (\text{II.B.3})$$

where  $r_{vol}$  and  $r_{sur}$  are the volume and surface residuals respectively, or,

$$r_{vol} = - \frac{1}{R} \left\{ \frac{\partial}{\partial R} \left( K \frac{\partial \psi}{\partial R} \right) + \frac{\partial}{\partial z} \left( K \frac{\partial \psi}{\partial z} \right) + f \right\} = 0 \quad (\text{II.B.4})$$

$$r_{sur} = \frac{1}{R} \left\{ K \frac{\partial \psi}{\partial n} + \alpha_1 (\psi - \psi_0) \right\} \quad (\text{II.B.5})$$

If the solution to equation (II.B.1) was exact, both  $r_{vol}$  and  $r_{sur}$  would be equal to zero.

In order to clarify the boundary condition, equation (II.B.2), one may analyze the equation as follows.



On the surface,  $S$ , where  $\psi$  is specified,

$$\psi = \psi_0 \quad (\text{II.B.6})$$

and,

$$\alpha_1 \rightarrow \infty \quad (\text{II.B.7})$$

Similarly, on the surface, where  $\frac{\partial \psi}{\partial n} = 0$ ,  $S_2$ , where

$$\alpha_1 = 0 \quad (\text{II.B.8})$$

$$S_1 \cap S_2 = \emptyset, \quad S_1 \cup S_2 = S \quad (\text{II.B.9})$$

Due to the axi symmetric assumption, the final equation will not involve  $dV$  and  $dS$  but the intersection of  $dV$  and  $dS$  with the meridional plane. Therefore, one must transform the volume integral,  $dV$ , to a surface integral and the surface integral,  $dS$ , to a line integral.

Hence, let,

$d\Omega$  = intersection of  $dV$  and meridional plane

$dC$  = intersection of  $dS$  and meridional plane

and,

$$dV = 2\pi R d\Omega$$

$$dS = 2\pi R dC$$

With this transformation, one may rewrite equation





(II.B.3) as follows,

$$\int_{\Omega} -W(R,z) \left[ \frac{\partial}{\partial R} \left( K \frac{\partial \psi}{\partial R} \right) + \frac{\partial}{\partial z} \left( K \frac{\partial \psi}{\partial z} \right) + f \right] 2\pi d\Omega + \int_C W(R,z) K \frac{\partial \psi}{\partial n} 2\pi dC = 0 \quad (\text{II.B.10})$$

where on the contour,  $C, \psi = \psi_0$ .

One must now integrate the first term in equation (II.B.10) by parts to obtain the following,

$$\begin{aligned} & - \int_{\Omega} W \left[ \frac{\partial}{\partial R} \left( K \frac{\partial \psi}{\partial R} \right) + \frac{\partial}{\partial z} \left( K \frac{\partial \psi}{\partial z} \right) \right] 2\pi d\Omega - \int_{\Omega} W \cdot f d\Omega \\ & + \int_{\Omega} K \left[ \frac{\partial \psi}{\partial R} \frac{\partial W}{\partial R} + \frac{\partial \psi}{\partial z} \frac{\partial W}{\partial z} \right] d\Omega + \int_C W K \frac{\partial \psi}{\partial n} 2\pi dC = 0 \end{aligned} \quad (\text{II.B.11})$$

Inspecting the first term in equation (II.B.11), one may use the following integral theorem to simplify further

$$\int_{\Omega} \partial_{\beta} \phi d\Omega = \int_C \phi n_{\beta} dC \quad (\text{II.B.12})$$

Rewriting equation (II.B.11) gives,

$$\begin{aligned} & - \int_C W K \left[ \frac{\partial \psi}{\partial R} n_R + \frac{\partial \psi}{\partial z} n_z \right] dC - \int_{\Omega} W f d\Omega + \int_{\Omega} K \left[ \frac{\partial \psi}{\partial R} \frac{\partial W}{\partial R} + \frac{\partial \psi}{\partial z} \frac{\partial W}{\partial z} \right] d\Omega \\ & + \int_C W K \frac{\partial \psi}{\partial n} 2\pi dC = 0 \end{aligned} \quad (\text{II.B.13})$$

Finally, since

$$\frac{\partial \psi}{\partial n} = \frac{\partial \psi}{\partial R} n_R + \frac{\partial \psi}{\partial z} n_z \quad (\text{II.B.14})$$

equation (II.B.13) reduces to the following,



$$\int_{\Omega} \left[ K \left( \frac{\partial \psi}{\partial r} \frac{\partial W}{\partial r} + \frac{\partial \psi}{\partial z} \frac{\partial W}{\partial z} \right) - f W \right] d\Omega = 0 \quad (\text{II.B.15})$$

One now has the final equation in the form for use by the weighted residual method using any arbitrary weighting function,  $W(r,z)$ . As noted previously, the Galerkin's Method will be used here which implies that the weighting functions are the same functions used in approximating the stream function,  $\psi$ .

Before applying the finite element method, one must discretize the continuum and then approximate the unknown function,  $\psi$ , by a set of polynomials. For this particular problem, eight-noded iso-parametric elements were chosen for discretization, see Fig 4, and the following approximating functions were used.

$$\psi = \sum_{i=1}^8 N_i(\xi, \eta) \psi_i \quad (\text{II.B.16})$$

where,

$N_i(\xi, \eta)$  = shape functions

$\psi_i$  = value of  $\psi$  at the node

$\psi$  = value of  $\psi$  at any arbitrary location within the element. The shape functions,  $N_i$ , used here are defined by the following relations as shown in Ref.10,



$$N_i(\xi, \eta) = \frac{1}{4}(1 + \xi\xi_i)(1 + \eta\eta_i)(\xi\xi_i + \eta\eta_i - 1)$$

$$N_i(\xi, \eta) = \frac{1}{2}(1 - \xi^2)(1 + \eta\eta_i) \quad (\text{II.B.17})$$

$$N_i(\xi, \eta) = \frac{1}{2}(1 + \xi\xi_i)(1 - \eta^2)$$

where the following coordinate transformations are used,

$$r = \sum_{i=1}^8 N_i(\xi, \eta) r_i \quad (\text{II.B.18})$$

$$z = \sum_{i=1}^8 N_i(\xi, \eta) z_i$$



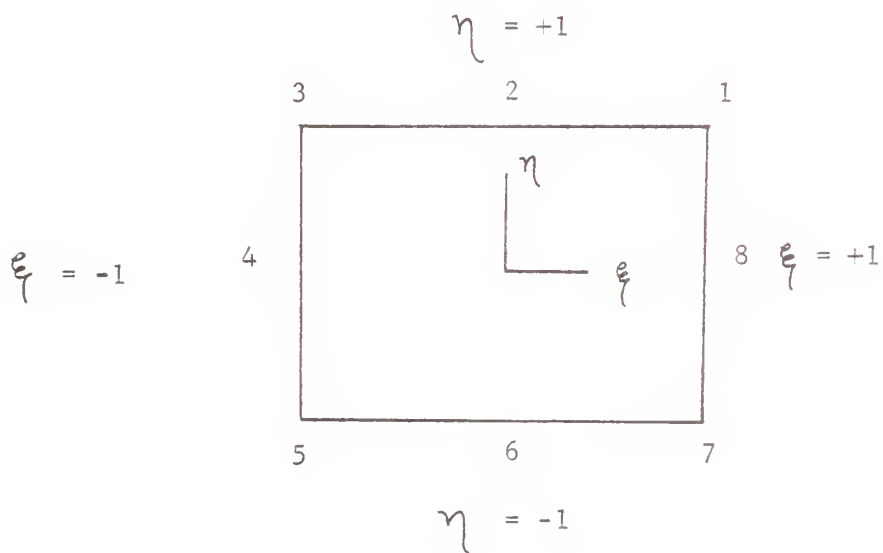
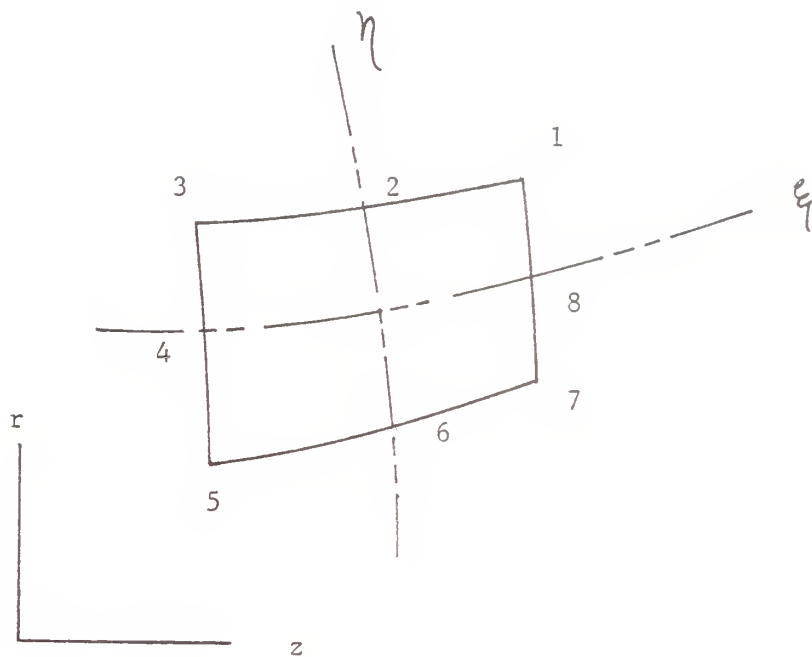


Figure 4 - ISOPARAMETRIC QUADRILATERAL ELEMENT





At this point, one is ready to apply the Galerkin Method to equation (II.B.15) by substituting equation (II.B.16) for the unknown function  $\psi$ , and  $N_i$  for the weight function,  $W$ , which yields,

$$\int_{\Omega} k \left\{ \frac{\partial N_i}{\partial r} \sum_{j=1}^8 \psi_j \left( \frac{\partial N_j}{\partial r} \right) + \frac{\partial N_i}{\partial z} \sum_{j=1}^8 \psi_j \left( \frac{\partial N_j}{\partial z} \right) \right\} d\Omega - \int_{\Omega} f_i N_i d\Omega = 0 \quad (\text{II.B.19})$$

This integration yields the following system of equations which is solved for the unknown nodal  $\psi$ ,

$$\begin{bmatrix} K_{11} & K_{12} & \cdots & K_{1n} \\ \vdots & & & \\ K_{n1} & \cdots & K_{nn} \end{bmatrix} \begin{Bmatrix} \psi_1 \\ \vdots \\ \psi_n \end{Bmatrix} = \begin{Bmatrix} f_1 \\ \vdots \\ f_n \end{Bmatrix} \quad (\text{II.B.20})$$

where,

$$K_{ij} = \int_{\Omega} k \left\{ \frac{\partial N_i}{\partial r} \frac{\partial N_j}{\partial r} + \frac{\partial N_i}{\partial z} \frac{\partial N_j}{\partial z} \right\} d\Omega \quad (\text{II.B.21})$$

and,

$$f_i = \int_{\Omega} f \cdot N_i d\Omega \quad (\text{II.B.22})$$

In addition since both the 'stiffness matrix',  $K$ , and the right hand side vector,  $[F]$ , are functions of  $\psi$ , the system as defined by equations (II.B.20) through (II.B.21) must be solved iteratively.

At this point one has the total finite element formulation of the radial equilibrium equation as defined by equations (II.B.19) and (II.B.20). The problems which remain to be clarified are basically two fold. Firstly one



must evaluate the integrals in equations (II.B.19) and (II.B.2) by numerical methods, and secondly, the solution procedure for the non-linearity must be formulated. In Part C, both of these final steps are presented.

## C. NUMERICAL INTEGRATION OF STIFFNESS MATRIX AND SOLUTION PROCEDURE

### 1. Numerical integration of the stiffness matrix

As noted in Section II.B, evaluation of equation (II.B.21) must be performed numerically. In addition, one realizes that the derivative expressions enclosed within the interval must be evaluated by a coordinate transformation. This is done in the following way,

Since,

$$r = \sum_{i=1}^8 N_i(\xi, \eta) r_i$$

$$z = \sum_{i=1}^8 N_i(\xi, \eta) z_i$$
(II.C.1)

then,

$$\frac{\partial N_i}{\partial \xi} = \frac{\partial N_i}{\partial z} \frac{\partial z}{\partial \xi} + \frac{\partial N_i}{\partial r} \frac{\partial r}{\partial \xi}$$

$$\frac{\partial N_i}{\partial \eta} = \frac{\partial N_i}{\partial z} \frac{\partial z}{\partial \eta} + \frac{\partial N_i}{\partial r} \frac{\partial r}{\partial \eta}$$
(II.C.2)



and in matrix form,

$$\begin{pmatrix} \frac{\partial N_i}{\partial \xi} \\ \frac{\partial N_i}{\partial \eta} \end{pmatrix} = \begin{bmatrix} \frac{\partial z}{\partial \xi} & \frac{\partial r}{\partial \xi} \\ \frac{\partial z}{\partial \eta} & \frac{\partial r}{\partial \eta} \end{bmatrix} \begin{pmatrix} \frac{\partial N_i}{\partial z} \\ \frac{\partial N_i}{\partial r} \end{pmatrix} \quad (\text{II.C.3})$$

Furthermore, defining the Jacobian matrix as,

$$J = \begin{bmatrix} \frac{\partial z}{\partial \xi} & \frac{\partial r}{\partial \xi} \\ \frac{\partial z}{\partial \eta} & \frac{\partial r}{\partial \eta} \end{bmatrix} \quad (\text{II.C.4})$$

then by dividing both sides of equation (II.C.3) by  $J$ , one has the following transformation,

$$\begin{pmatrix} \frac{\partial N_i}{\partial z} \\ \frac{\partial N_i}{\partial r} \end{pmatrix} = [J]^{-1} \begin{pmatrix} \frac{\partial N_i}{\partial \xi} \\ \frac{\partial N_i}{\partial \eta} \end{pmatrix} \quad (\text{II.C.5})$$

In addition, it has been shown [Ref.9] that

$$dzdr = |J| d\xi d\eta \quad (\text{II.C.6})$$

Now, with equations (II.C.5) and (II.C.6), equation (II.B.21) becomes the following,



$$K_{ij} = \int_{-1}^1 \int_{-1}^1 K \left[ \frac{\partial N_i}{\partial \xi} \frac{\partial N_j}{\partial \eta} \right] \{ [J]^{-1} \}^T [J]^{-1} \left\{ \frac{\partial N_i}{\partial \xi} \right\} \left\{ \frac{\partial N_j}{\partial \eta} \right\} \det [J] d\xi d\eta \quad (\text{II.C.7})$$

Equation (II.C.7) is best integrated using the Gauss-Legendre integration method since it is of the following form,

$$K_{ij} = \int_{-1}^1 \int_{-1}^1 G(\xi, \eta) d\xi d\eta \quad (\text{II.C.8})$$

or finally, [Ref.10],

$$K_{ij} = \sum_{i=1}^2 \{ A_i B_i f(\xi_i, \eta_i) \} \quad (\text{II.C.9})$$

where  $A_i$  and  $B_i$  are coefficients (Fig 5) for both two and three point Gaussian Quadrature.

At this point, one has the tools to calculate all the elements of the stiffness matrix. In like manner, the right hand side vector,  $f$ , is calculated by numerical integration.





NUMBER OF GAUSS IAN POINTS	$\pm \eta$ $\pm \xi$	$\pm A_i$ $\pm B_i$
2	0.57735 02691	1.00000 00000
3	0.77459 66692 0.00000 00000	0.55555 55555 0.88888 88888

Figure 5 - GAUSSIAN INTEGRATION POINTS



## 2. Solution procedure

The following is a synopsis of the basic solution process. Specific details concerning equations and methods of computer coding are covered in the proceeding section. The proceeding is meant to give the reader a preview of the solution process.

### a. Discretization

Initially the machine under analysis is discretized into eight-node iso-parametric elements. The axial calculation stations are placed arbitrarily in the duct regions and along blade edges and centers for the rotor and stator as shown in Fig 6. At this point the system topology and nodal coordinates are specified.

### b. Initialization

To begin the iteration process, one must assume an initial internal stream function, velocity, and density distribution. In the program, the initial internal stream function was assumed to be that of the outer boundary throughout while the velocity and density distribution was assumed to be that of the inlet.



COMPUTED WORK 1

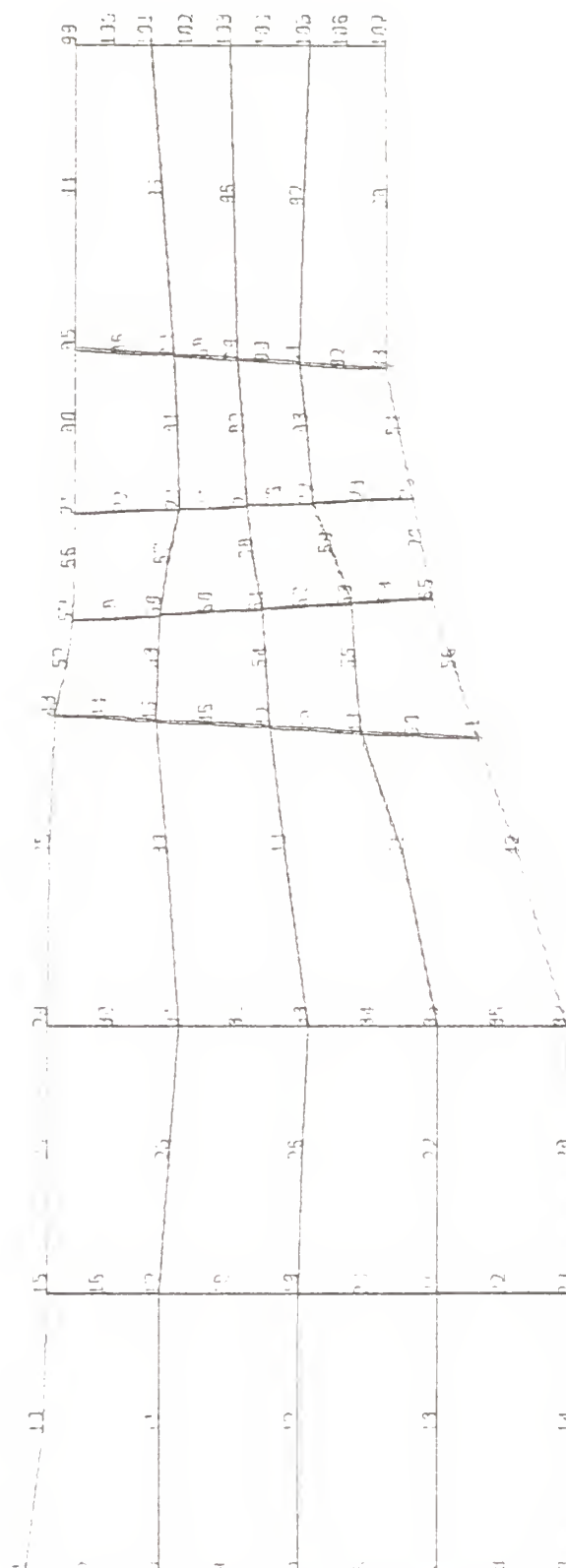


Figure 6 - COMPRESSOR DISCRETIZATION



### c. Calculation of thermodynamic variables

Before calculating the right-hand side vector,  $f$ , one must obtain distributions of angular momentum, enthalpy, and entropy. This is done by first calculating the thermodynamic variables at the inlet axial station from the given inlet conditions. In order to proceed axially through the machine to calculate the nodal angular momentum, enthalpy, and entropy, the following three equations derived in Section III are used.

$$H = C_p T = \text{constant along a stator streamline}$$

$$H_R = C_p T_{tr} - \frac{(wr)^2}{2} = \text{constant along a rotor streamline}$$

$$r V_\theta = \text{constant along a duct streamline}$$

An example of this calculation procedure for the duct region is shown graphically in Fig 7.





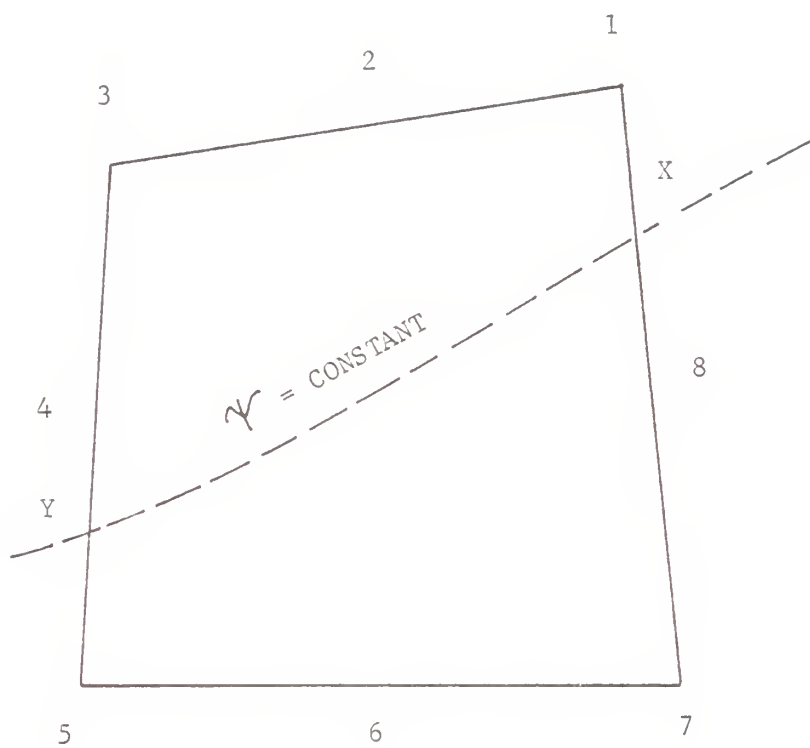


Figure 7 - DUCT ELEMENT



In this figure, the angular momentum at point X is equal to the angular momentum at point Y. More formally,

$$(rV_{\theta})_x = \sum_{i=3}^5 N_i(\xi, \eta) (rV_{\theta})_i = (rV_{\theta})_y \quad (\text{II.C.2.1})$$

Since the previous axial station's thermodynamic variables are known, one must now find the values of  $\xi$  and  $\eta$  at point Y. This is done iteratively in the following way. Since

$$\psi|_Y = \psi|_x = \sum_{i=3}^5 N_i(\xi, \eta) \psi_i \quad (\text{II.C.2.2})$$

and along the left side of the element,

$$\xi = -1 \quad (\text{II.C.2.3})$$

then equation (II.C.2.2) may be solved for  $\eta$  by a suitable iteration method. As will be shown in the next section, a half-interval method was used to obtain the unknown  $\eta$ . Once  $\eta$  is known, then equation (II.C.2.1) is solved for the angular momentum at point X. The rotor and stator are handled in a similar fashion. In addition, the rotor and stator deviate the flow creating a three-dimensional flow field between the blades in the respective blade row. Low speed cascade correlation data [Ref.13] was used to calculate the effective turning angles in the rotor and stator. These effects are calculated beforehand with known mass flow rate and uniform axial velocity assumptions at the rotor inlet. The results of these calculations are part of the input data routine in the form of relative and absolute flow angles at the rotor nodes and absolute flow angles at



the stator nodes. This will be shown more exactly in the next section.

d. Calculate matrices

At this point, the right hand side vector,  $f$ , and the stiffness matrix,  $K$ , are calculated.

e. Solve system of equations

The system of equations as shown in equation (II.B.20) is solved for the nodal stream function.

f. Perform relaxation iteration

Due to the strong non-linear properties of the system of equations, the following iterative scheme is necessary.

$$\psi_i^{n+1} = \psi_i^n + \alpha [\hat{\psi}_i^{n+1} - \psi_i^n] \quad (\text{II.C.2.4})$$

where  $\alpha$  is the under relaxation factor. As will be shown in Section III, this scheme is performed only in certain regions of the machine and in addition after a specified number of iterations.

g. Update velocity and density profiles

Using the current nodal distribution of the stream function, axial and radial nodal velocity components are calculated along with a new nodal density distribution.



Again, this calculation procedure will be shown in the next section.

#### h. Test for convergence of $\psi$

Stream function convergence criteria is now tested and will determine if further iterations are necessary. The solution is said to converge if the following equation holds for all nodes.

$$\left| \frac{\psi_i^n - \psi_i^{n+1}}{\psi_i^{n+1}} \right| < \epsilon \quad (\text{II.C.2.5})$$

where  $\epsilon$  is a designated requirement for convergence.

#### i. Summary

In summary, the eight steps involved in the solution are noted below;

(1) Discretize the continuum.

(2) Assume an initial stream function, velocity, and density solution.

(3) Calculate the nodal thermodynamic variables from the given inlet conditions.

(4) Form the right hand side vector,  $f(r,z)$ , and the stiffness matrix,  $K$ .

(5) Solve the system of equations, given by,  $[K] = [F]$  for a new stream function distribution.





(6) Perform relaxation iteration if required.

(7) Calculate new nodal velocity and density distributions from the current stream function solution.

(8) Test the solution for convergence, and if required, repeat steps (3) through (8) using the current nodal stream function values.

This concludes the solution description and now one is ready to more completely understand the computer program which assembles the preceding eight steps.



### III. THE PROGRAM

#### A. OVERALL FLOWCHART AND DESCRIPTION

The overall flowchart of the program is depicted in Fig 8. Those blocks denoted by the letter 'S' are subroutines, while the remaining calculations are an integral part of the main program.

After proper dimensioning of all arrays and subsequent initialization, the input data are read and then printed. This not only presents a physical picture of the problem but also serves as a cross check to the user for correct data insertion. In addition, a subroutine is available to obtain a computer drawn plot of the mesh (Fig 6) and is a further check on proper data input.

At this point all the necessary variables have been stored and the iteration counter for stream function convergence is set. With the current nodal values of  $\psi$  and the given inlet thermodynamic conditions, the thermodynamic variables throughout the machine are calculated. From the calculated values of enthalpy and angular momentum, (isentropic flow is assumed), the right-hand side vector is calculated followed by the stiffness matrix calculation (equation II.B.21).

The system of equations (equation (II.B.20)) is now solved for the new nodal stream function distribution. It is here where for all iterations but the first that a



relaxation factor is applied as noted previously in equation (II.C.2.4). The reasoning behind not applying the relaxation scheme to the value of nodal  $\Psi$  after the first iteration is the fact that the first iteration produced a close approximation to the correct stream function distribution. With this close approximation to the stream function came a velocity and density distribution which in turn was near the correct solution. It was found that if the first iteration was relaxed, the second iteration became unstable since in fact the velocities and densities were themselves farther from the true values than were assumed initially.

After testing the nodal stream function for convergence by use of equation (II.C.2.5), the calculation process is either repeated or ceased by virtue of convergence or limiting the number of iterations.

As stated previously, low speed cascade correlation data [Ref.13] were used to calculate turning angles in the blade regions. These angles were assumed constant throughout the solution and not refined after subsequent iterations. Further work on the computer program could entail an additional computational routine which would calculate the new turning angles after each iteration. A sample calculation of rotor turning angles is shown in Appendix D.

In the following sections the program structure is examined in more detail.



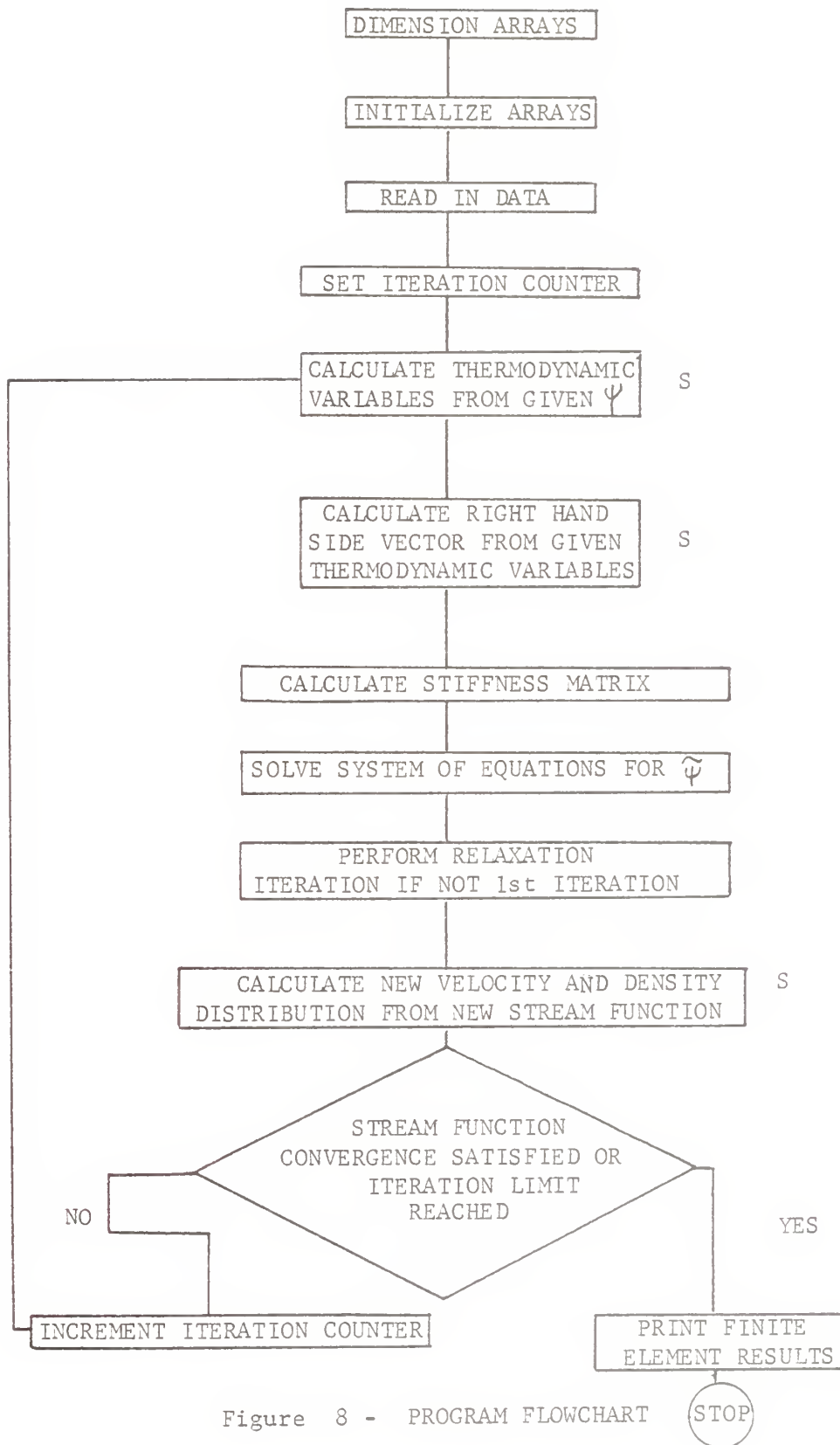


Figure 8 - PROGRAM FLOWCHART





## B. THE MAIN PROGRAM

### 1. The input routine

The following is a description of the input data required by the program. The data are arranged into twelve categories described in the following manner.

#### a. category 1

Problem identification.

#### b. category 2

Number of nodes and number of elements.

#### c. category 3

Node numbers, nodal coordinates and nodal blockage factor.

#### d. category 4

System topology.

#### e. category 5



Element type; duct, rotor, or stator.

f. category 6

Absolute flow angles for rotor and stator nodes.

g. category 7

Relative flow angles for rotor nodes.

h. category 8

Inlet thermodynamic quantities.

i. category 9

Physical constants for fluid under observation.

j. category 10

First estimate of internal stream function.

k. category 11

Node numbers and specified nodal stream  
function.

l. category 12



Node numbers where the right hand side,  $f(r,z)$ , is to be calculated.

Before describing in detail the format to be followed for data insertion, it is important to note the following assumptions.

(1) Uniform flow conditions at inlet and outlet.

(2) Uniform flow conditions at rotor inlet for calculation of appropriate turning angles. This assumption is necessary to calculate the values of rotor and stator flow angles.

With this in mind , the discussion will continue.

The following describes each category in more detail.

Category 1:

Format: (20A4)

Number of cards: 1

Procedure: Enter the title of the problem in columns 1-20.

Category 2:

Format: (2I10)

Number of cards: Equal to the number of nodes in the system.



Procedure: Enter the number of nodes in columns 1-10, and the number of elements in 11-20. Both integers must be right justified.

Category 3:

Format: (I10,3F10.0)

Number of cards: Equal to the number of nodes in the system.

Procedure: Each card contains the node number followed by the Z coordinate, R coordinate, and nodal blockage factor. The coordinates are in dimensions of inches.

Category 4:

Format: (9I5)

Number of cards: Equal to the number of elements in the system.

Procedure: Each card contains nine integers right justified in columns 5, 10, 15, etc., through 45. The first integer is the element number followed by the eight nodes associated with that element. It is important to note that the nodes are read in starting with the upper right hand node and proceeding in a counterclockwise fashion around the element.

Category 5:

Format: (2I10)

Number of cards: Equal to the number of





elements.

Procedure: Enter the element number in columns 1-10, followed by the integer '1' (duct), '2' (rotor), or '3' (stator) describing the element as either in a duct, rotor, or stator region.

Category 6:

Format: (6X,A4,I 10,F10.0)

Number of cards: Equal to the number of rotor and stator nodes plus one 'STOP' card.

Procedure: Enter the node number (right justified) in columns 11-20 followed by the value of the associated absolute flow angle in radians in columns 21-30. The last card in this category is a 'STOP' card entered in columns 7-10.

Category 7:

Format: (6X,A4,I 10,F10.0)

Number of cards: Equal to the number of rotor nodes plus one 'STOP' card.

Procedure: Enter the node number (right justified) in columns 11-20 followed by the value of the associated relative flow angle in radians in columns 21-30. The last card in this category is a 'STOP' card.

Category 8:

Format: (7F10.0), (F10.0)



Number of cards: 2

Procedure: Enter the following quantities in the prescribed order and with the noted dimensions.

First card

Mass flow rate: (lbm/sec)

Inlet axial velocity: (ft/sec)

Outlet axial velocity: (ft/sec)

Inlet total density: (lbm/ft<sup>3</sup>)

Inlet static density: (lbm/ft<sup>3</sup>)

Inlet total pressure: (lbf/in<sup>2</sup>)

Inlet total temperature: (°R)

Second card

Speed: (RPM)

Category 9:

Format: (3F10.0)

Number of cards: 1

Procedure: Enter the following quantities in the prescribed order.

Gas constant: (ft-lbf/lbm-°R)



Ratio of specific heats

Constant pressure specific heat:  
(BTU/lbm-°R)

Category 10:

Format: (F10.0)

Number of cards: 1

Procedure: Enter the first estimate of the internal stream function to be used in the first iteration.

Category 11:

Format: (6X,A4,I10,F10.0)

Number of cards: Equal to the number of nodes having a specified value of the stream function plus a 'STOP' card.

Procedure: This set of cards allows the stream function boundary conditions to be read in. A typical card contains an integer, right justified in columns 11-20 , which is the node number, followed by the value of the specified stream function in columns 21-30. The last card is a 'STOP' card.

Category 12:

Format: (6X,A4,I10)

Number of cards: Equal to the number of nodes where the right hand side is to be specified.



Procedure: Enter the node number, right justified in columns 11-20, where the right hand side is to be calculated. Again, the last card in this category is a 'STOP' card.

After all the data has been read by the program, the input data is printed and the mesh is plotted for verification by the user. The sample format is shown in Appendix C.

This concludes the input routine. The next section describes the calculation of the stiffness matrix, K.

## 2. Stiffness matrix evaluation

As shown previously in Section II.C.1, the following equation describes each term in the eight by eight elemental matrix.

$$K_{ij} = \int_{-1}^1 \int_{-1}^1 k \left[ \frac{\partial N_i}{\partial \xi} \frac{\partial N_j}{\partial \eta} \right] \{ [J]^{-1} \}^T \{ \} \det [J] d\xi d\eta \quad (\text{III.B.2.1})$$

In addition, 'k' is defined in the following way in order to numerically integrate the equation.

$$k = \frac{1}{\sum_{i=1}^8 p_i N_i(\xi, \eta) \cdot \sum_{i=1}^8 r_i N_i(\xi, \eta) \cdot \bar{b}} \quad (\text{III.B.2.2})$$

where b is defined as the elemental blockage factor taken as an average over the eight nodes of the particular element and  $(\xi, \eta)$  are the defined Gauss-Quadrature integration points.





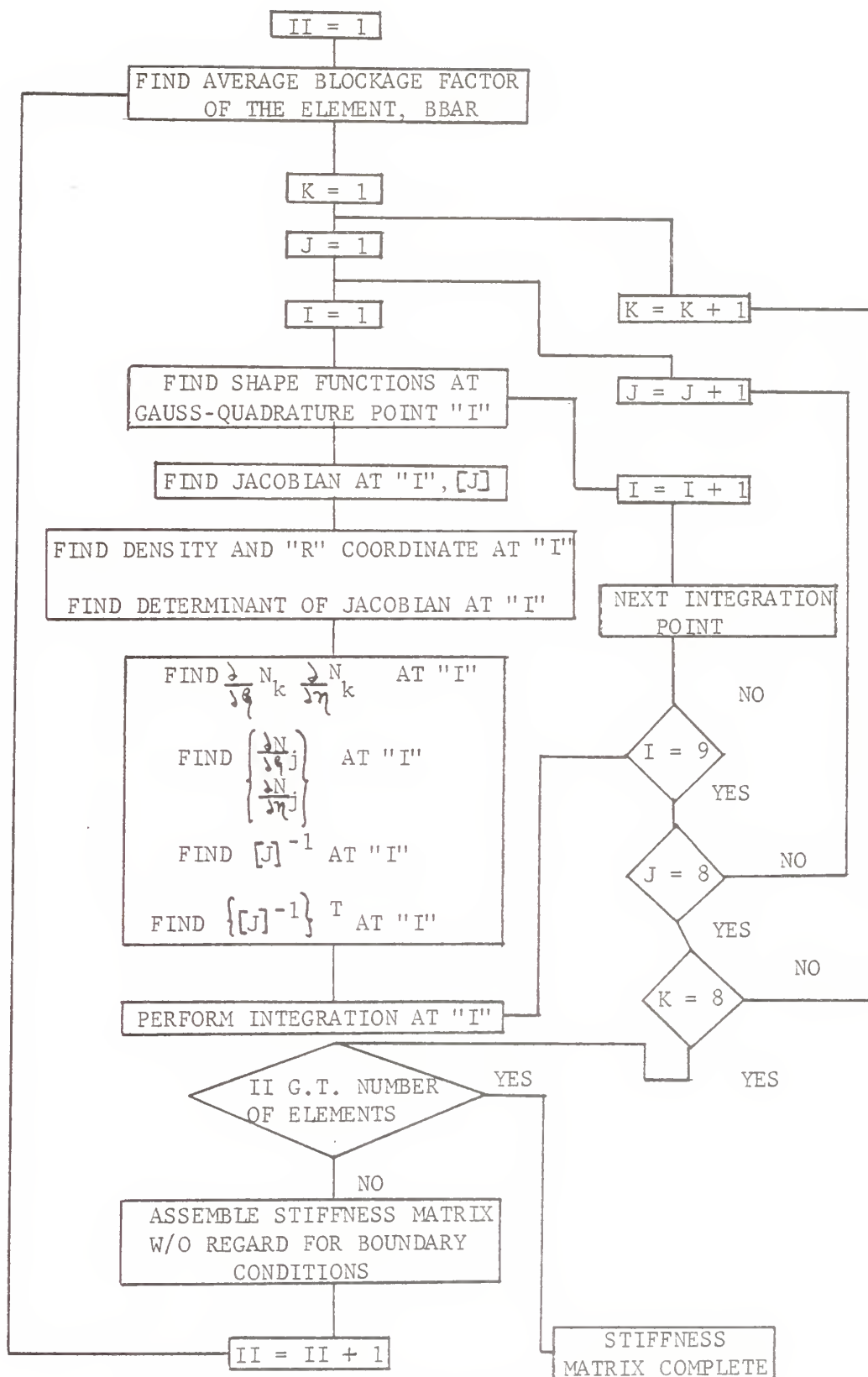


Figure 9 - STIFFNESS MATRIX EVALUATION



Fig 9 depicts the flowchart for both elemental stiffness matrix evaluation and the assemblage into the system stiffness matrix. More specifically, the figure shows a three-point Gaussian Quadrature scheme but can be changed to a two-point scheme by simply integrating four times instead of nine as shown.

The actual coding of the stiffness matrix evaluation and assemblage may be found in lines STR03510 through STR04770 in the computer program.

### 3. Solution of systems of equations

At this point, the system of equations are modified for the boundary conditions and solved for the nodal stream function values. An equation solving routine, DSIMQ, available in the system library was used for this purpose. It was found that no comparable savings was realised by using a banded equation solver.

### 4. Iteration schemes

As noted previously in Section II.C, a relaxation scheme is necessary for convergence to a solution.

Two distinct differences with regard to the iteration method were noted from that of Ref.7. Firstly, it was found that relaxation was necessary only in the rotor and stator elements and also in the duct region between the rotor outlet and stator inlet. Secondly, due to the extreme non linearity in the rotor-stator areas, a switch was required which changed the sign of  $\alpha$  in equation (II.C.2.4) as required for stability of convergence. Clarification of



this change follows: It was found that during the initial three or four iterations, the stream function values of the rotor-stator nodes sometimes exceeded the value of the upper boundary. Due to an absence of sources within the domain of solution, this occurrence was incompatible with the boundary conditions. At this point, it was necessary to make  $\alpha$  negative in equation (II.C.2.4). During subsequent iterations, as the solution converged, the rotor-stator regions became stable and the sign of  $\alpha$  was returned to its positive value. This iteration proved to stabilize the solution with respect to stream function values and velocities.

The iteration procedure is coded in the computer program from lines STR05070 through STR05200.

#### 5. The output routine

Once convergence is obtained or the number of iterations have reached the limit imposed by the user, the results are displayed. A sample output is shown in the Appendix. In addition, the units of all dependent variables are the same as those noted in the input routine.

### C. THE SUBROUTINES

The following describes each of the six subroutines in the computer program. Each subsection contains a list of calling arguments and for subroutines FCAL, SLINE, and VEL, a basic flowchart. In addition, for those subroutines whose mathematical theory was not presented in Section III, a brief treatment is also given.



## 1. Subroutine shape

This subroutine calculates the shape functions (equation (II.B.17)) at the values of  $\xi$  and  $\eta$  as requested in the argument list below.

SUBROUTINE SHAPE (E,Z,SF)

E = value of  $\xi$  (input)

Z = value of  $\eta$  (input)

SF = eight by one vector of the eight shape functions.

## 2. Subroutine jacob

JACOB calculates the Jacobian matrix as defined in equation (II.C.1.4) for the value of  $\xi, \eta$  denoted in the argument list.

SUBROUTINE JACOB (E1,Z1,D,E,RC\$,ZC\$,RJAC)

E1 = value of  $\eta$  (input)

Z1 = value of  $\xi$  (input)

D = eight by one vector of  $\frac{\partial N_i}{\partial \xi}$  (calculated)

E = eight by one vector of  $\frac{\partial N_i}{\partial \eta}$  (calculated)

RC\$ = eight by one vector of the 'r' coordinates of the nodes associated with the element (input)

ZC\$ = eight by one vector of the 'z' coordinates of the nodes associated with the element (input)

RJAC = two by two Jacobian matrix (output)





In addition, the subroutine assumes that the vectors RC\$ and ZC\$ contain element coordinates arranged in a counter clockwise fashion beginning with the upper right corner node.

### 3. Subroutine sline

This subroutine calculates the thermodynamic variables throughout the machine given the inlet conditions as described in Section II.C.2. The calling arguments are defined below.

```
SUBROUTINE SLINE(UINLET,RC,PSI,WRL,H,UVEL,VVEL,TVEL,  
NODE,NNODEI,CP,TT,KK,ALP,WG,TWEL,BE,HS)
```

UINLET = Inlet axial velocity

RC = Nodal 'r' coordinates vector

PSI = Nodal stream function vector

WRL = Nodal angular momentum vector

H = Nodal total enthalpy vector

UVEL = Nodal axial velocity vector

VVEL = Nodal radial velocity vector

TVEL = Nodal absolute tangential velocity vector

NODE = Matrix containing nodes associated with the element

INLET = Vector containing node numbers at inlet station

NNODEI = Number of nodes at inlet station

CP = Specific heat

TT = Total temperature at inlet



KK = Iteration counter

NTE = Element type vector

ALP = Nodal absolute flow angle vector

TWEL = Nodal relative tangential velocity vector

BE = Nodal relative flow angle vector

HS = Nodal static enthalpy vector

As shown in Fig 10, the basic calculation procedure begins with calculating the required energy and momentum values at the inlet station. At this point, beginning with element one, the element type is interrogated to distinguish between duct, rotor, and stator elements. If the element is in a duct region, then the streamline intersections for local nodes 2,6,7,8 and 1 (Fig 7) are determined along with the associated values of energy and angular momentum. For the rotor and stator elements, one must initially find the energy and momentum values at local nodes 3,4,5 (Fig 7) due to the discontinuities imposed by the blade edges. Once these calculations are performed, then the process for the remaining nodes in the element proceeds in a similar fashion to the duct elements.

After all the elements have been cycled through, the new distributions of nodal angular momentum and energy are returned to the main program for further computations. Specifically, these values will be used by the next subroutine, FCAL, for calculation of the right hand side vector.



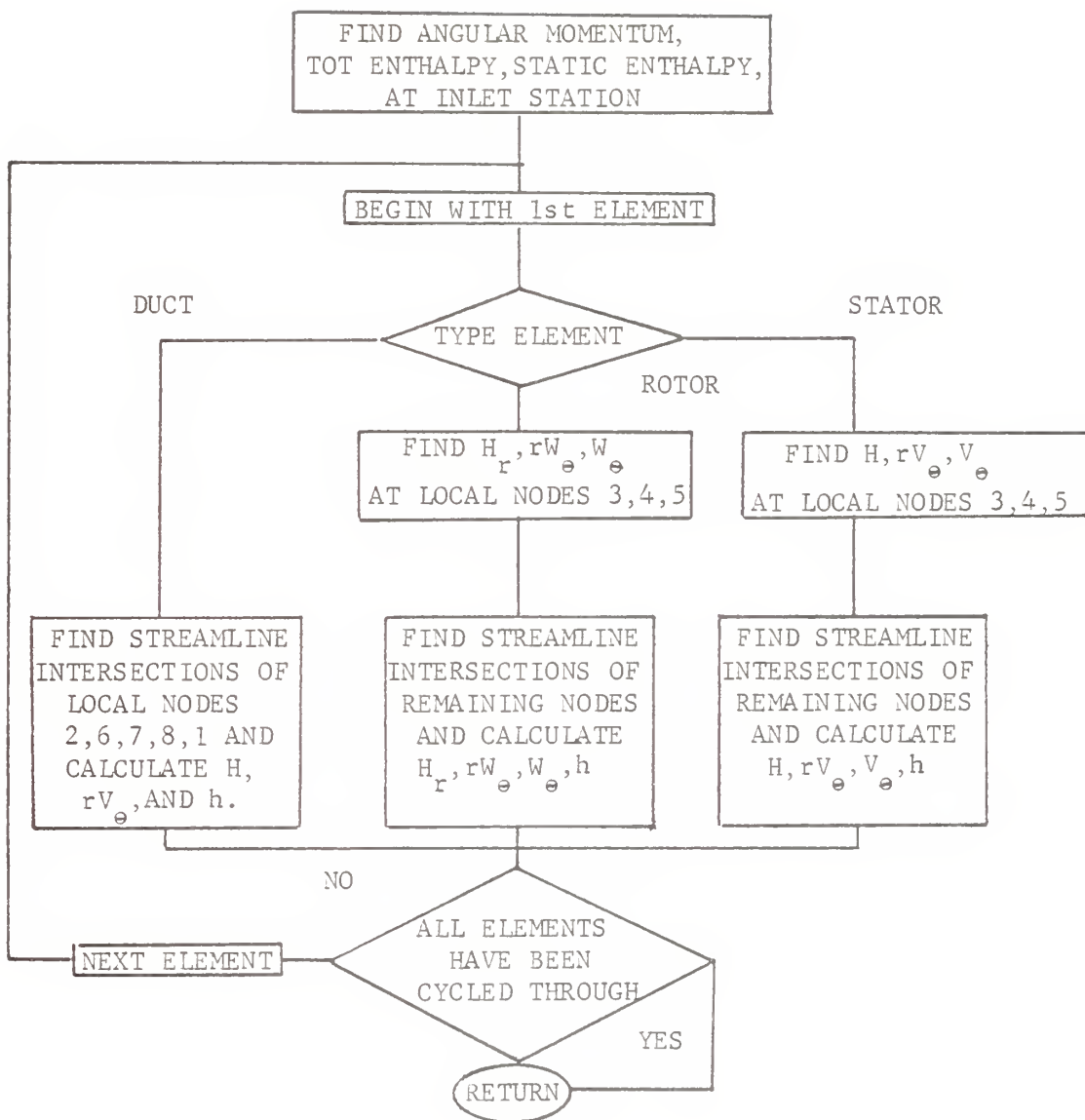


Figure 10 - SUBROUTINE SLINE



#### 4. Subroutine fcal

FCAL calculates the right hand side vector as defined by equations (II.A.31) and (II.B.21). Using the identical coordinate transformations - for numerical integration as described in Section II.C, the final equation to be coded is the following,

$$f_i = \int_{-1}^1 \int_{-1}^1 \frac{N_i}{\sum N_i V_{zi}} \cdot \frac{\sum N_i V_{\theta i}}{\sum N_i R_i} \left\{ \left( L J^{-1}(z, 1) \cdot \frac{\partial N_i}{\partial \xi} + J(z, 2) \cdot \frac{\partial N_i}{\partial \eta} \right) (W_i - H_i) \right\} \det J d\xi d\eta \quad (\text{III.C.4.1})$$

where isentropic flow is assumed, and,

$W_i$  = angular momentum

(III.C.4.2)

$H_i$  = total enthalpy

The argument list is defined below. In addition, only those variables in the list which have not been defined previously are described.

SUBROUTINE FCAL(F,W,H,ZA,EA,UVEL,RC,ZC,WRL,TVEL,NFS,  
,NODE,NN,NE,NFSP,TWEL,NFE)

F = Right hand side vector,  $f(r, z)$

W = vector of gaussian quadrature coefficients

ZA = Vector of  $\xi$ ; gaussian quadrature points

EA = Vector of  $\eta$ ; gaussian quadrature points

NFS = Vector containing nodes where the right hand side





is to be specified

NN = number of nodes

NE = number of elements

NNFSP = Number of nodes where the right hand side is specified

Fig 11 depicts the basic flowchart for the subroutine. To initialize the procedure, one begins with the first node (upper right hand corner) of the first element. A switch is then applied which determines if the right hand side is to be calculated at the node or if a stream function value has been specified. This information is transferred from the main program through the argument list. Once the node is allowed through the switch, then the integration process is started at the first integration point. As in Section III.A.2, the flowchart depicts a three-point Gauss Quadrature scheme. After the integration has been completed, a switch determines if all the local nodes in the element have been cycled through and if so, then the assembly of the elemental vector,  $F_s$ , is performed to build the system right hand side vector,  $F$ . Finally, the subroutine determines if all the elements have been examined in order to signal completion of the right hand side vector. At this point, the vector,  $F(r,z)$ , is returned to the main program for problem solution.



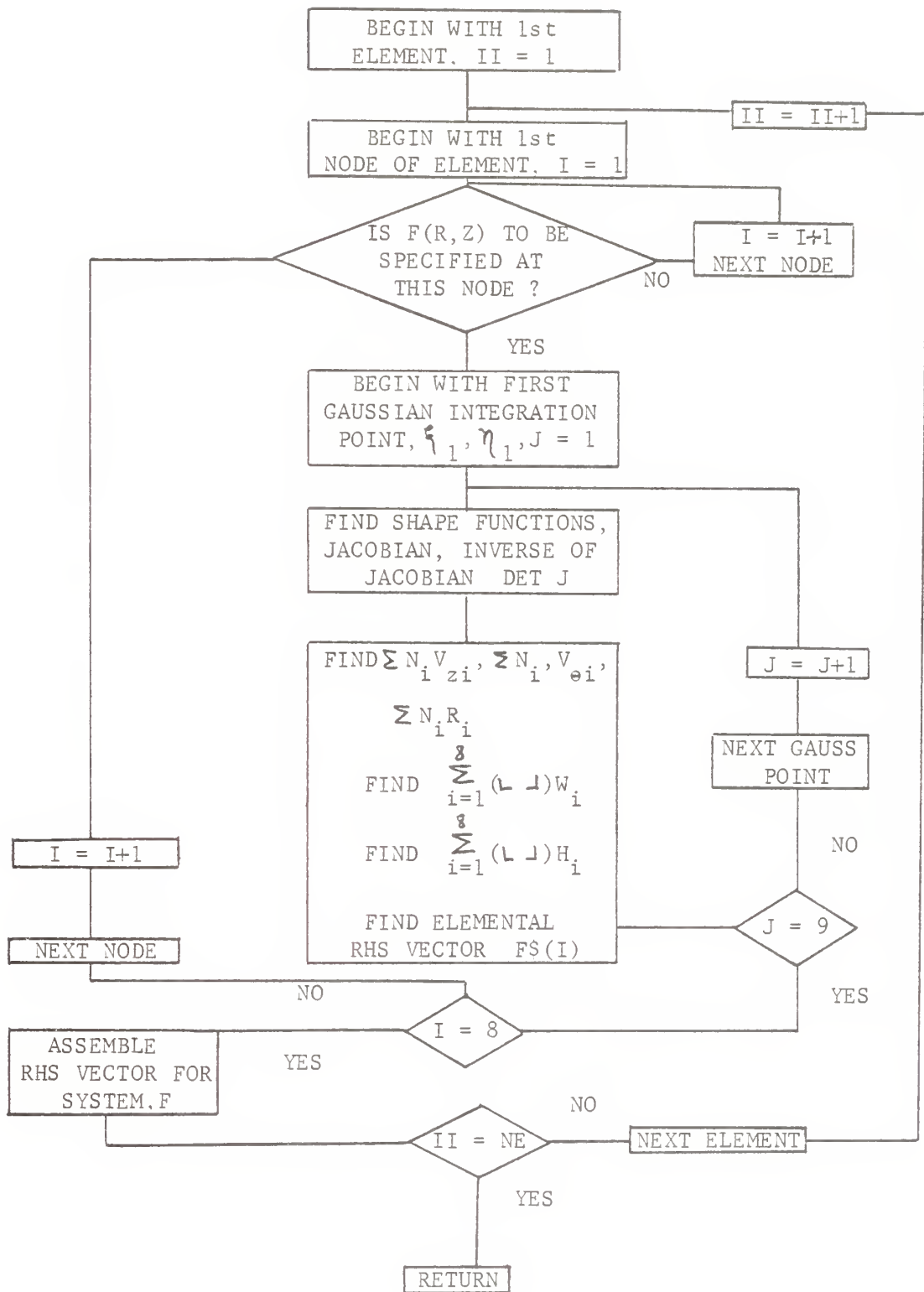


Figure 11 - SUBROUTINE FCAL



## 5. Subroutine vel

This subroutine calculates axial and radial velocities and also densities at each of the nodes from a known stream function distribution. As noted previously in Section II.C.2, both velocity and density profiles are updated after obtaining the latest value of nodal stream function.

The velocity calculation proceeds from the stream function equations,

$$V_z = \frac{1}{\rho r b} \frac{\partial \psi}{\partial r} \quad (\text{III.C.5.1})$$

$$V_r = - \frac{1}{\rho r b} \frac{\partial \psi}{\partial z} \quad (\text{III.C.5.2})$$

where 'b' is the tangential blockage factor. Since  $r$ ,  $\rho$ , and  $\psi$  are of the following form,

$$\begin{aligned} r &= \sum_{i=1}^8 r_i N_i \\ \rho &= \sum_{i=1}^8 \rho_i N_i \\ \psi &= \sum_{i=1}^8 N_i \psi_i \end{aligned} \quad (\text{III.C.5.3})$$

then the equation for the axial velocity,  $V_z$ , becomes,

$$V_z = \frac{1}{b \sum_{i=1}^8 \rho_i N_i \sum_{i=1}^8 N_i r_i} \left[ \sum_{i=1}^8 \frac{\partial N_i}{\partial r} \psi_i \right] \quad (\text{III.C.5.4})$$

Again, since the shape function,  $N_i(\eta, \eta)$ , is not an



implicit function of 'r' and 'z', one must use equation (II.C.1.5) to obtain the proper derivatives for computation of equation (III.C.5.4). For example, from equation (III.C.5),

$$\sum_{i=1}^8 \frac{\partial N_i}{\partial r} = \sum_{i=1}^8 \left[ J^{-1}(1,1) \cdot \frac{\partial N_i}{\partial \xi} + J^{-1}(1,2) \frac{\partial N_i}{\partial \eta} \right] \quad (\text{III.C.5.5})$$

At this point, with equation (III.C.5.5) substituted into equation (III.C.5.4), one has the complete expression for the axial velocity as functions of  $\xi, \eta$ . One proceeds similarly for expressing the radial velocity,  $V$ , in terms of  $\xi$  and  $\eta$ .

In order to calculate the nodal density, one uses the following density relation for flows in the stator and duct regions.

$$\frac{\rho}{\rho_t} = \left( 1 - \frac{\gamma-1}{2a_0} V^2 \right)^{\frac{1}{\gamma-1}} \quad (\text{III.C.5.6})$$

where  $\rho_t$  is the stagnation density.

Since,

$$V^2 = (V_z^2 + V_r^2) (1 + \tan^2 \alpha) \quad (\text{III.C.5.7})$$

then,

$$\frac{\rho}{\rho_t} = \left[ 1 - \frac{\gamma-1}{2a_0} \left( \frac{1}{r b} \right)^2 (\psi_r^2 + \psi_z^2) (1 + \tan^2 \alpha) \right]^{\frac{1}{\gamma-1}} \quad (\text{III.C.5.8})$$





Since the density appears on both sides of the equation, the new nodal density is obtained iteratively at the node.

For the relative flows in the rotor, the following relation for static density is used [Ref.14].

$$\frac{\rho}{\rho_t} = \left[ 1 - (\gamma-1) \frac{\omega R V_\theta}{a_o^2} - \frac{(\gamma-1)}{2} \frac{W^2 - \omega^2 R^2}{a_o^2} \right]^{\frac{1}{\gamma-1}} \quad (\text{III.C.5.9})$$

Again, the solution of the nodal density is obtained in an iterative fashion.

In the following argument list, only those variables not defined in the previous subroutine descriptions are noted.

SUBROUTINE VEL(NE, NN, RC, NODE, G, RG, TT, RHOT, RHON, ZC, PSI, RHO, B, UINLET, UVEL, VVEL, RHOSTA, NTE, ALP)

G = Ratio of specific heats

RG = Gas constant

RHOT = Total density at the inlet

RHON = Work vector which contains the new nodal density distribution

RHO = Nodal static density vector

B = nodal blockage factor vector

RHOSTA = Static density at the inlet station

The basic flowchart for SUBROUTINE VEL is shown in Fig 12. Beginning with the first node of the first element, the Jacobian matrix (equation (II.C.1.4)) and its inverse



are found. At this point the partial derivatives with respect to 'r' and 'z' of the shape functions are found as noted in equation (III.C.5.5). A switch then allows those nodes not at the inlet station to pass and calculates the new density and velocities at the nodes. For those nodes at the inlet, the velocities and static densities are retained at the given inlet conditions. This is done to maintain boundary condition integrity for the solution. After cycling through all elements, the subroutine returns the new nodal velocity and density distributions to the main program.



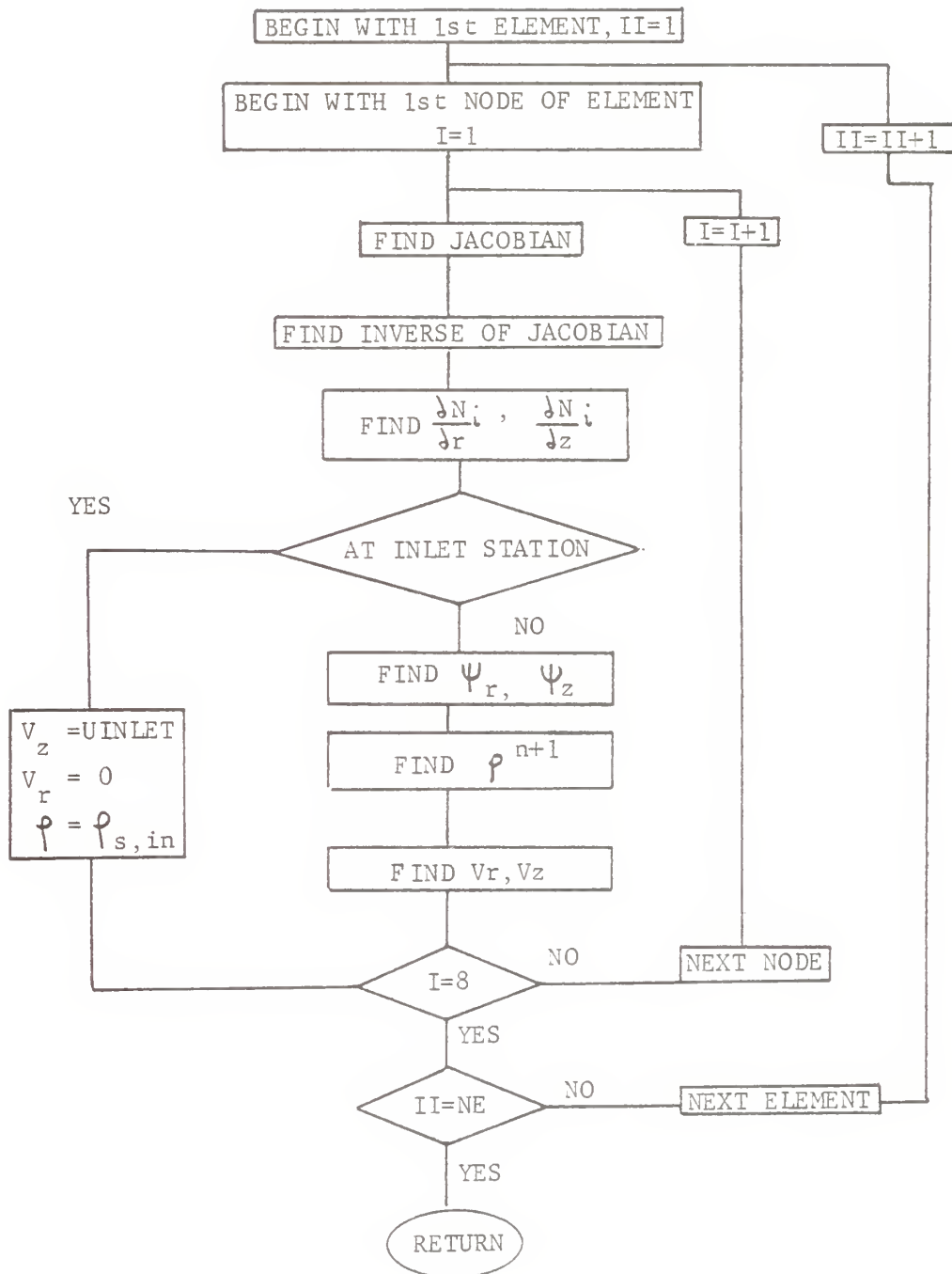


Figure 12 - SUBROUTINE VEL



## 6. Subroutine mplot

This subroutine utilizes the Calcomp plotter to depict the mesh topology of the machine under observation.

```
SUBROUTINE MPlot(RC,ZC,NODE,NN,NE)
```

This completes the description of the main program and associated subroutines. In the next section, a test case is carried through from data input to final results.





#### IV. TEST CASES AND RESULTS

The program was tested by using published performance data [Ref.12] of the NASA Task-1 stage transonic compressor. The compressor was discretized into twenty-eight elements and 107 nodes with 15 axial calculation stations (Fig 6). The speed was 0.5 design speed with a mass flow of 107.6 lbm/sec. In addition, uniform flow was assumed both at the inlet and outlet stations. Turning angles for the rotor and stator were pre calculated assuming uniform conditions at the rotor inlet and using NASA SP-36 blade correlation data [Ref.13]. These absolute and relative flow angles were assumed constant throughout the iterative procedure as they were an integral part of the input data. The Appendix contains a listing of the input data and output results for the NASA Task-1 transonic compressor with test conditions noted. To compare the accuracy of the predicted flow with actual laboratory observations, computed axial velocity profiles at the rotor inlet, rotor outlet, stator inlet, and stator outlet were compared with experimental results. In addition numerical results from Ref.7 were also compared.

Fig 13-16 show the computer predictions plotted with the experimental values and the numerical solutions obtained by Hirsch and Warzee. The profiles shown were obtained after ten iterations and using a relaxation factor of 0.2. The figures show that the best overall agreement with experimental data occurred in the stator inlet and outlet. In this region the worst error was 17% which occurred at the stator tip inlet. The average error throughout the stator region with respect to experimental data was 6.6%.



The rotor hub and tip outlet area exhibited instabilities in density convergence using equation III.C.5.9. Specifically, the density solution converged to within 8% at the rotor outlet tip and hub. It was found that by not allowing the nodal density at these nodes to go below a critical value of 0.06 lbm/cu ft, the solution for the stream function converged. By allowing the nodal densities at the rotor outlet tip and hub to go below this critical value, the computed velocities at these nodes became increasingly large and the argument within the brackets of equation III.C.5.9 became less than one. This prevented continuation of the iterations for the stream function solution. In addition, the rotor tip outlet exhibited more instability than the rotor hub outlet. The static density at the rotor hub outlet oscillated about a value of 0.062 lbm/cu ft while the rotor tip outlet was constantly driven to the critical value of 0.06 lbm/cu ft. One method attempted to alleviate this problem was the following. Since a half-interval iteration routine was used, one trial run involved reversing the direction of consecutive guesses when the density iteration did not converge. It was found however, that after three to four iterations of the system of equations, the static densities at the rotor outlet tip and hub were again driven to smaller and smaller values which led to instability once more. The nodal densities converged at all interior points of the rotor edge and mid-blade regions and also at all the rotor inlet nodes. By including all rotor nodes, the average error with respect to experimental data was 27.5%.

Fig 17 shows a plot of convergence criteria,  $\epsilon$ , versus the number of iterations for a relaxation factor of 0.2. The stability of convergence is shown to initially decrease and then after the third iteration oscillates about an approximate value of 28%. It is important to note that this curve represents the maximum value of  $\epsilon$  as shown in equation



(II.C.2.5). In addition, the curve in actuality represents the oscillation of nodal stream function values in the rotor/stator regions since in fact this is where the non-linearity is the greatest.



## V. CONCLUSIONS AND RECOMMENDATIONS FOR FURTHER STUDY

Agreement with both experimental data and numerical solution of Ref.7 was best in the stator region to within 8%. Predicted axial velocity profiles in the rotor inlet area were within 26.2% of experimental results. The instabilities with respect to static density solutions are prevalent. One of the reasons for this numerical disagreement with Hirsch and Warzee is the isentropic assumption imposed by the present program. Recommendations for further study on the project include the addition of entropy variations in the rotor and stator blade regions. This would necessitate the use of blade correlation data [Ref.13] for loss predictions and involve additional input data plus program additions to Subroutine's SLINE and FCAL.





RADIUS (IN)

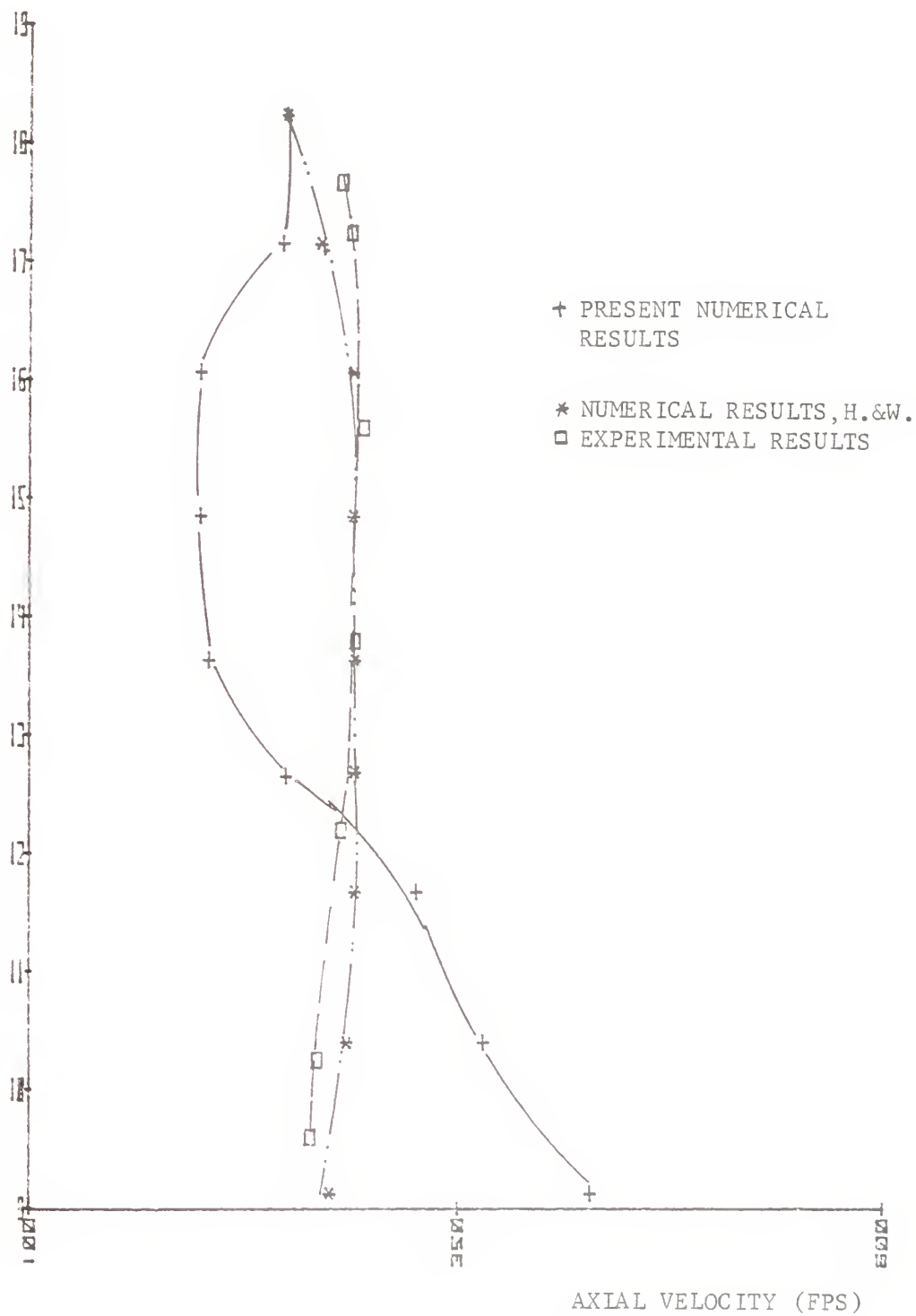


Figure 13 - AXIAL PROFILE AT ROTOR INLET



RADIUS (IN)

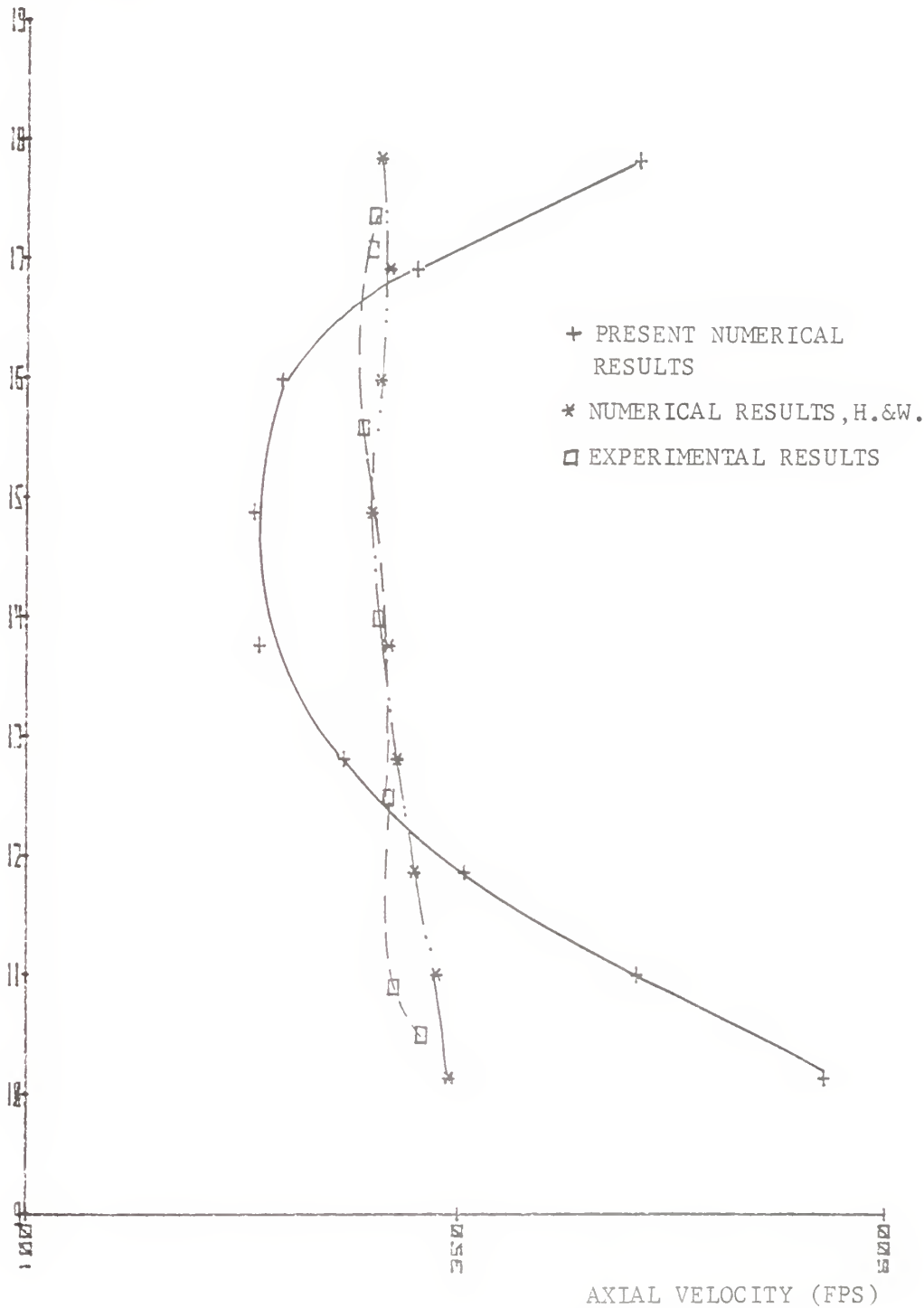


Figure 14 - AXIAL PROFILE AT ROTOR OUTLET



RADIUS (IN)

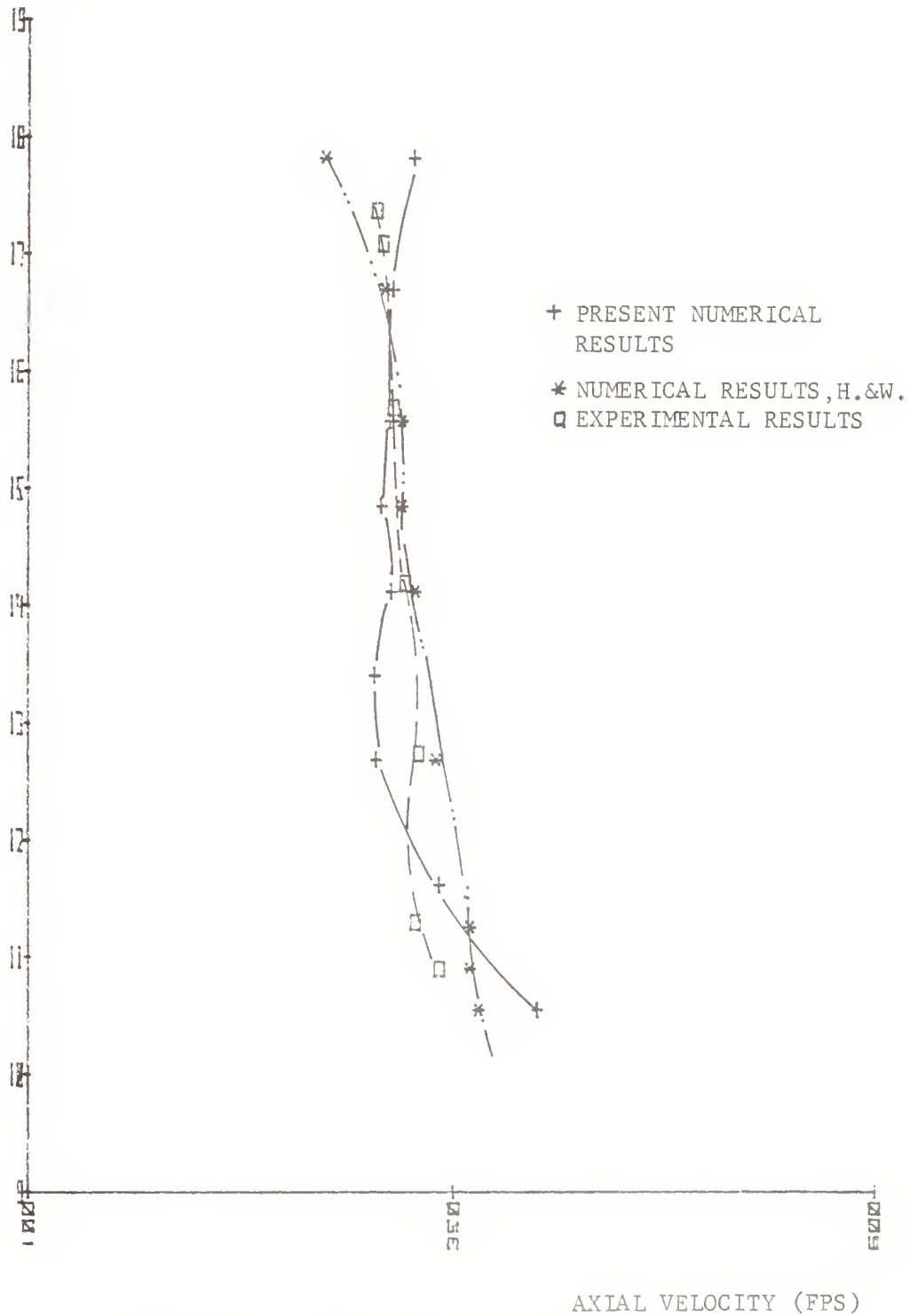


Figure 15 - AXIAL PROFILE AT STATOR INLET



RADIUS (IN)

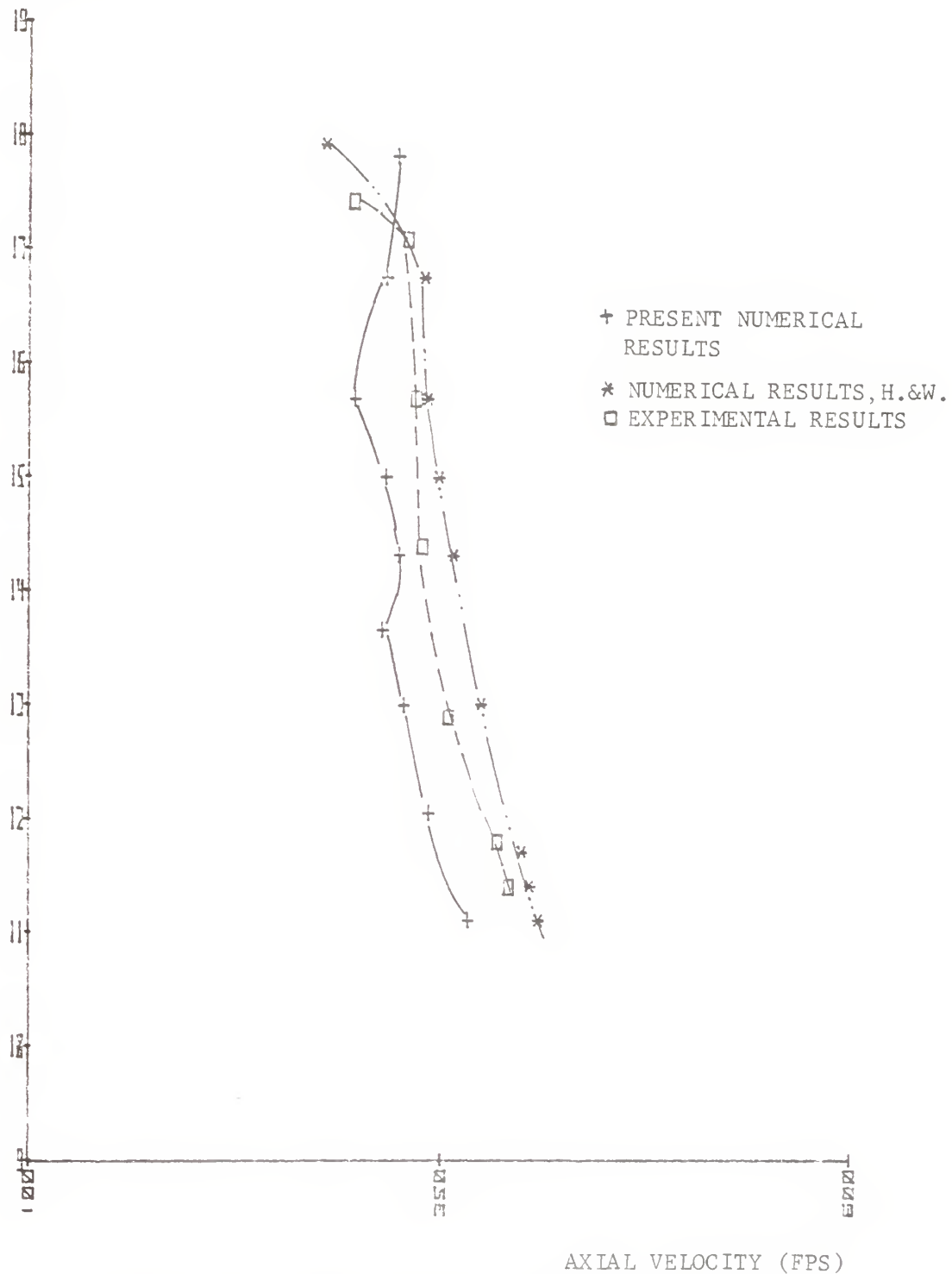


Figure 16 - AXIAL PROFILE AT STATOR OUTLET





EPSILON

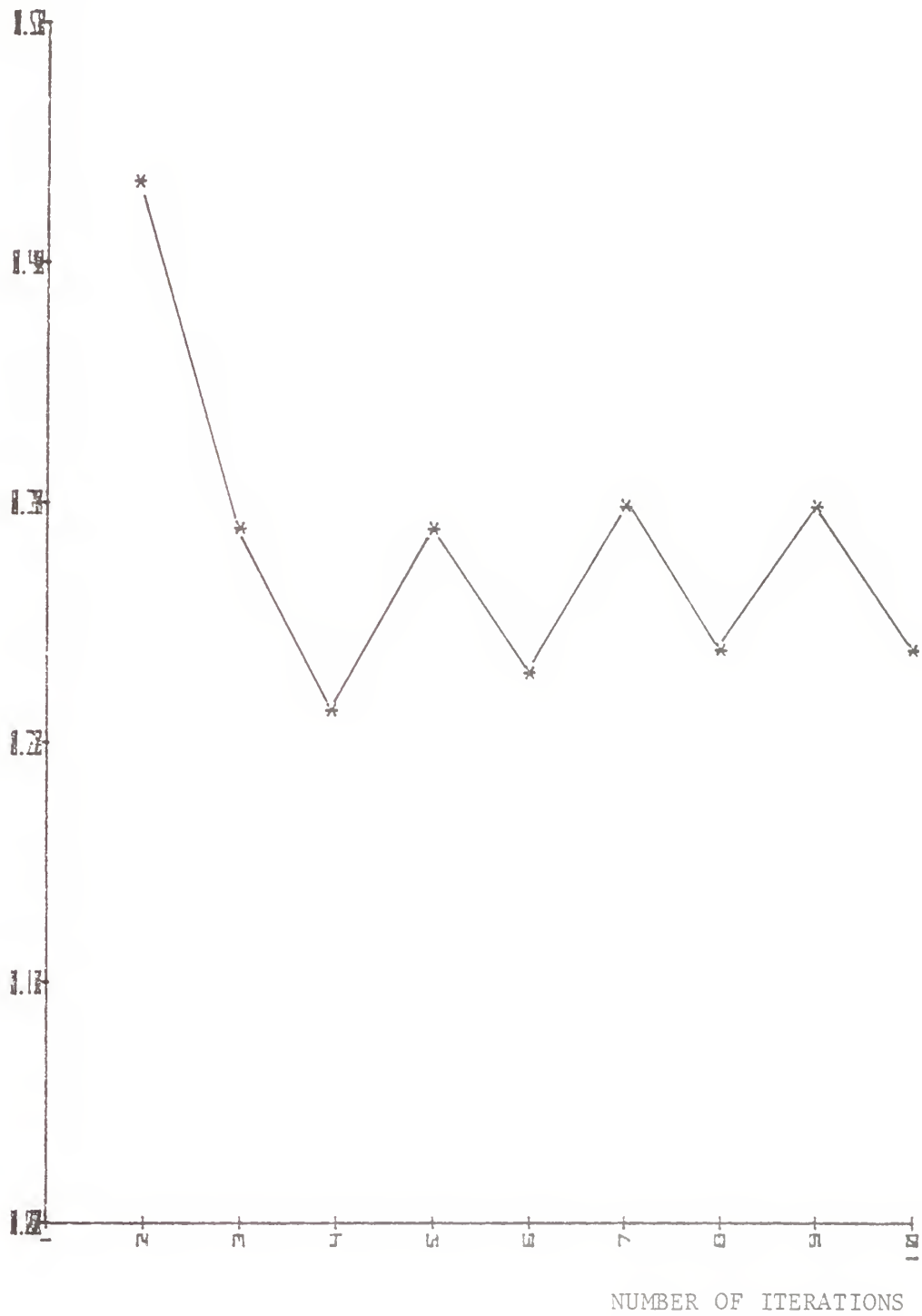


Figure 17 - EPSILON VS. ITERATIONS



## APPENDIX A

### COMPUTER PROGRAM

```
C THE FINITE ELEMENT METHOD APPLIED TO TWO-DIMENSIONAL.
C AXI-SYMMETRIC, INVISCID, COMPRESSIBLE FLOW IN A TURBO-
C MACHINE. STREAM FUNCTION FORMULATION IS USED ALONG WITH
C EIGHT-NODE ISOPARAMETRIC ELEMENTS. TWO POINT OR THREE
C POINT GAUSSIAN QUADRATURE FOR NUMERICAL INTEGRATIONS
C ARE USED.
```

```
      IMPLICIT REAL*8(A-H,P-Z)
      DATA NREAD/4/,
            DATA NWRITE/7/,
            DATA STOP/'STOP' /
```

```
      DIMENSION ALL ARRAY VARIABLES

      DIMENSION RJAC(2,2), ROW(1,2), COL(2,1), EM$(8,8), RIJAC(2,2), R(40)
      DIMENSION FM(107,107), F(107), PSI(107), RHS(107), TIJAC(2,2)
      DIMENSION PROD1(1,2), PRD2(1,2), PRD3(1,1), FNZ1(1,1), FNZ2(1,1), W(9)
      DIMENSION D(8), SF(8), ZA(9), EA(9), RHOF(40)
      DIMENSION UVFL(107), VVEL(107), PRES(107), RC$(8)
      DIMENSION ZC$(8), RC(107), ZC(107), RHO(107), B(107), RHON(107)
      DIMENSION WRL(107)
```

```
      TVFL(107), PSIO(107), H(107), ALP(107), TWEL(107), BE(107)
      RTEMP(107), HS(107)
      DIMENSION NPSSI(107), NFIS(107)
      DIMENSION NFS(107), NPSI(107), NNDE(28,8), NI(2), MI(2), INLET(10)
      DIMENSION IULET(10), NTE(40), ITITLE(10)
```

```
TWO-POINT GAUSSIAN POINTS.

DATA ZA/.57735027D0,-.57735027D0,-.57735027D0,.57735027D0/
DATA EA/.57735027D0,.57735027D0,-.57735027D0,-.57735027D0/
```

```
THREE-POINT GAUSSIAN POINTS.

DATA ZA/.774596669242D0,.774596669242D0,.7774596669242D0,
1.0D0,0.D0,0.D0,-.774596669242D0,-.774596669242D0,
2-.774596669242D0/
DATA EA/.774596669242D0,0.D0,-.774596669242D0,
1.774596669242D0,0.D0,-.774596669242D0,
2.774596669242D0,0.D0,-.774596669242D0/
WEIGHTING FUNCTIONS FOR 3 PT. GAUSSIAN QUAD. PTS.

DATA W/.3086419752D0,.4938271604D0,.3086419752D0,
1.4938271604D0,.7901234566D0,.4938271604D0,
2.3086419752D0,.4938271604D0,.3086419752D0/
```

```
CC READ IN TITLE
CC READ(NREAD,50)ITITLE
```



```

50      FORMAT(10A4)
C
C
C
C
100
C
      READ IN NUMBER OF NODES AND NUMBER OF ELEMENTS

      READ(NREAD,100) NN,NE
      FORMAT(2I10)
      INITIALIZE ALL MATRICES
      DO 110 I = 1,NN
      F(I) = 0.00
      PSI(I) = 0.00
      RHS(I) = 0.00
      NPSIS(I) = 0
      UVEL(I) = 0.00
      VVEL(I) = 0.00
      TVEL(I) = 0.00
      PRES(I) = 0.00
      RC(I) = 0.00
      ZC(I) = 0.00
      B(I) = 0.00
      NFS(I) = 0
      NPSI(I) = 0
      WRL(I) = 0.00
      RHO(I) = 0.00
      RHCN(I) = 0.00
      H(I) = 0.00
      HS(I) = 0.00
      ALP(I) = 0.00
      TWEL(I) = 0.00
      BE(I) = 0.00
      CONTINUE
      ZEROIZE OUT INLET( ) AND IULET( )
      DO 111 I = 1,10
      INLET(I) = 0
      IULET(I) = 0
      CONTINUE
      DO 140 I = 1,2
      ROW(I,1) = 0.00
      COL(I,1) = 0.00
      PROD1(I,1) = 0.00
      PROD2(I,1) = 0.00
      CONTINUE
      DO 150 I = 1,NN
      DO 150 J = 1,NN
      EM(I,J) = 0.00
      CONTINUE
      DO 160 I = 1,8
      DO 160 J = 1,8
      STR00490
      STR00500
      STR00510
      STR00520
      STR00530
      STR00540
      STR00550
      STR00560
      STR00570
      STR00580
      STR00590
      STR00600
      STR00610
      STR00620
      STR00630
      STR00640
      STR00650
      STR00660
      STR00670
      STR00680
      STR00690
      STR00700
      STR00710
      STR00720
      STR00730
      STR00740
      STR00750
      STR00760
      STR00770
      STR00780
      STR00790
      STR00800
      STR00810
      STR00820
      STR00830
      STR00840
      STR00850
      STR00860
      STR00870
      STR00880
      STR00890
      STR00900
      STR00910
      STR00920
      STR00930
      STR00940
      STR00950
      STR00960

```



160	EM\$(I,J) = 0.D0	STR00970
	CONTINUE	STR00980
	DO 165 I = 1, NE	STR00990
	NTE(I) = 0	STR01000
	RHOE(I) = 0.D0	STR01010
	R(I) = 0.D0	STR01020
	DO 165 J = 1, 8	STR01030
	NODE(I,J) = 0	STR01040
165	CONTINUE	STR01050
	READ NODE NUMBERS, NODAL COORDINATES (IN INCHES), AND NODAL BLOCKAGE FACTOR. INLET STATION ZC(I) MUST BE = 0.D0.	STR01060
	LAST NODAL ZC(NN) MUST BE AT THE OUTLET STATION.	STR01070
		STR01080
1000	DO 170 J = 1, NN	STR01090
170	READ(NR, 1000) I, ZC(I), RC(I), B(I)	STR01100
	FORMAT(110, 3F10.0)	STR01110
	CONTINUE	STR01120
	READ IN SYSTEM TOPOLOGY, I.E., ELEMENT NO. AND LOCAL NODE NUMBERS.	STR01130
	STARTING AT UPPER RIGHT HAND CORNER AND TRAVERSING IN A CCW	STR01140
	FASHION AROUND THE QUADRILATERAL.	STR01150
		STR01160
		STR01170
		STR01180
1010	DO 180 L = 1, NE	STR01190
180	READ(NR, 1010) J, NODE(J, 1), NODE(J, 2), NODE(J, 3), NODE(J, 4)	STR01200
	1, NODE(J, 5), NODE(J, 6), NODE(J, 7), NODE(J, 8)	STR01210
	FORMAT(9I5)	STR01220
	CONTINUE	STR01230
	READ IN TYPE OF ELEMENT: NTE(I)=1(DUCT), NTE(I)=2(ROTOR)	STR01240
	NTE(I)=3(STATOR)	STR01250
	DO 185 I = 1, NE	STR01260
	READ(NR, 1011) J, NTE(I)	STR01270
1011	FORMAT(2I10)	STR01280
185	CONTINUE	STR01290
	READ IN STATOR/ROTOR NODAL ABS FLOW ANGLES	STR01300
	REMEMBER THAT THIS ASSUMES UNIFORM FLOW CONDITIONS AT	STR01310
	ROTOR INLET.	STR01320
		STR01330
		STR01340
		STR01350
		STR01360
1012	DO 186 I = 1, NN	STR01370
	READ(NR, 1012) WORD, J, ANGLE	STR01380
	FORMAT(6X, A4, I10, F10.0)	STR01390
	IF(WORD.EQ.STOP) GOTO 1014	STR01400
	ALP(J) = ANGLE	STR01410
186	CONTINUE	STR01420
		STR01430
	READ IN ROTOR NODAL REL FLOW ANGLES.	STR01440









```

C      FINDING THE NNODES, PROCEED TO CALCULATE THE VALUES OF
C      PSI BY ASSUMING UNIFORM FLOW CONDITIONS AT INLET AND
C      OUTLET BY ASSUMING RHO = STATIC DENSITY AT INLET(RHOSTA)
C
C      FIND NODES AT INLET STATION
      KIS = 0
DO 231 I = 1, NN
  IF(ZC(I).NE.0.D0)GOTO231
  KIS = KIS + 1
  INLET(KIS) = I
  NNODEI = KIS
CONTINUE
231
C      FIND NODES AT OUTLET STATION
      KIS = 0
DO 232 I = 1, NN
  IF(ZC(I).NE.ZC(NN))GOTO232
  KIS = KIS + 1
  IULET(KIS) = I
  NNODEO = KIS
CONTINUE
232
C      READ NODES WHERE PSI IS SPECIFIED
      DO 190 I = 1, NN
      REAC(NR, I) = 1020
      WORD, NPSP, PS
      FORMAT(6X, A4, I10, F10.0)
      IF(WORD.EQ.STOP)GOTO191
      NPSP(I) = NPSP
      PSI(NPSP(I)) = PS
      PSIO(NPSP(I)) = PS
CONTINUE
190
C      COUNT NODES HAVING SPECIFIED PSI
      NNSPSI = I-1
      INSERT INLET PSI DISTRIBUTION FROM 'U' VEL DISTRIBUTION.
191
      DO 192 I = 1, NNODEI
      NPSPS(NNSPSI + I) = INLET(I)
      PSI(INLET(I)) = UINLET*(RC(INLET(I))**2 - RC(NNODEI)**2)/2.D0
      PSI(INLET(I)) = PSI(INLET(I))*RHO(INLET(I))/144.D0
      PSIO(INLET(I)) = PSI(INLET(I))
CONTINUE
192
      NNSPSI = NNSPSI + NNODEI
      INSERT OUTLET PSI DISTRIBUTION FROM 'U' VEL DISTRIBUTION
C
      DO 193 I = 1, NNODEO
      NPSPS(NNSPSI + I) = IULET(I)
      PSI(IULET(I)) = UOULET*(RC(IULET(I))**2 - RC(NN)**2)/2.D0
      PSI(IULET(I)) = PSI(IULET(I))*RHO(IULET(I))/144.D0
      PSIO(IULET(I)) = PSI(IULET(I))
CONTINUE
193

```



```

C          RECOUNT NUMBER OF NODES WITH SPECIFIED PSI BY INCLUDING
C          THE INLET AND OUTLET NODES.
C
C          NNSPSI = NNSPSI + NNODEO
C          READ NODES WHERE F(R,Z) IS SPECIFIED
1030      DO 200 I = 1,NN
          READ(NREAD,1030) WORD,NFSP
          FORMAT(6X,A4,I10)
          IF(WORD.EQ.STOP)GOTO201
          NPS(I) = NFSP
          CONTINUE
200      NNFSP = I-1
C
C          NFIS IS A LIST OF THE INDICES OF THE KNOWN F(R,Z)
C
C          DO 210 I = 1,NNFSP
          NFIS(I) = NPS(I)
          CONTINUE
210      C
C          NPSI IS A LIST OF THE INDICES IF THE KNOWN PSI
C
C          DO 220 I = 1,NNSPSI
          NPSI(I) = NPSIS(I)
          CONTINUE
220      C
C          NTOTF IS THE TOTAL NUMBER OF KNOWN F(R,Z)
C          NTOTF = NNFSP
C
C          NTOTP IS THE TOTAL NUMBER OF KNOWN PSI
C          NTOTP = NNSPSI
C          PRINT ALL INPUT DATA
C
C          GO TO 1101
221      WRITE(NWRITE,1038)TITLE
1038      FORMAT(1X,20X,10A4)
          WRITE(NWRITE,1040)NN,NE
1040      FORMAT(1X,4X,NO. OF NODES = 1,13,/,5X,
1*NO. OF ELEMENTS = 1,12)
          WRITE(NWRITE,1045)
1045      FCRMAT(1,1,20X,SUMMARY OF NODAL COORDINATES')
          WRITE(NWRITE,1050)
1050      FCRMAT(1,1,NODE,5X,Z(I),11X,R(I),11X,B(I)',
1*7X,ABS FLOW ANG,3X,REL FLOW ANG)
          WRITE(NWRITE,1060)(I,ZC(I),RC(I),B(I),ALP(I),BE(I),I=1,NN)
1060      FORMAT(1,1,13,2X,E13.6,2X,E13.6,2X,E13.6)
          WRITE(NWRITE,1062)
1062      FORMAT(1,1,20X,SYSTEM TOPOLOGY',/,2X,ELEMENT',
110X,NODES,40X,TYPE OF ELEMENT')
          WRITE(NWRITE,1063)(I,NODE(I,1),NODE(I,2),NODE(I,3),NODE(I,4)

```

```

STR02410
STR02420
STR02430
STR02440
STR02450
STR02460
STR02470
STR02480
STR02490
STR02500
STR02510
STR02520
STR02530
STR02540
STR02550
STR02560
STR02570
STR02580
STR02590
STR02600
STR02610
STR02620
STR02630
STR02640
STR02650
STR02660
STR02670
STR02680
STR02690
STR02700
STR02710
STR02720
STR02730
STR02740
STR02750
STR02760
STR02770
STR02780
STR02790
STR02800
STR02810
STR02820
STR02830
STR02840
STR02850
STR02860
STR02870
STR02880

```













```

C          CALCULATE JACOBIAN
C          CALL JACOB(EA(I),ZA(I),D,E,RC$,ZC$,RJAC)
C
C          FIND RHOE AND R FOR NUMERICAL INTEGRATION.
C
C          DO 330 L = 1,8
C             RHOE(I) = RHOE(I) + SF(L)*RHO(NODE(I,L))
C             R(I) = R(I) + SF(L)*RC(NODE(I,L))
C             CONTINUE
330
C          FIND DETERMINANT OF THE JACOBIAN.
C
C          DETJ = RJAC(1,1)*RJAC(2,2) - RJAC(1,2)*RJAC(2,1)
C          ROW(1,1) = D(K)
C          ROW(1,2) = E(K)
C          COL(1,1) = D(J)
C          COL(2,1) = E(J)
C          FIND INVERSE OF JACOBIAN
C          CALL OMINV(RJAC,2,A,L1,M1)
C
C          FIND TRANSPOSE OF INVERSE OF JACOBIAN
C
C          DO 340 I1 = 1,2
C             DO 340 J1 = 1,2
C                TIJAC(J1,I1) = RJAC(I1,J1)
C                CONTINUE
340
C          CALCULATE ROW*TRANSPOSE(INV J)
C
C          PROD1(1,1) = ROW(1,1)*TIJAC(1,1) + ROW(1,2)*TIJAC(2,1)
C          PROD1(1,2) = ROW(1,1)*TIJAC(1,2) + ROW(1,2)*TIJAC(2,2)
C
C          CALCULATE PROD1 * INV(J)
C
C          PROD2(1,1) = PROD1(1,1)*RJAC(1,1) + PROD1(1,2)*RJAC(2,1)
C          PROD2(1,2) = PROD1(1,1)*RJAC(1,2) + PROD1(1,2)*RJAC(2,2)
C
C          CALCULATE PROD2 * COL
C
C          PROD3(1) = PROD2(1,1)*COL(1,1) + PROD2(1,2)*COL(2,1)
C
C          MULTIPLY BY DET J
C
C          FNZ1(1) = DETJ*PROD3(1)
C          CALCULATE K = 1/(RHO*R*B)
C
C          ERHO = 1.0/(RHOE(I)*R(I)*BBAR)
C          CALCULATE FINAL INTEGRAL EXPRESSION
C

```

```

STR03840
STR03850
STR03860
STR03870
STR03880
STR03890
STR03900
STR03910
STR03920
STR03930
STR03940
STR03950
STR03960
STR03970
STR03980
STR03990
STR04000
STR04010
STR04020
STR04030
STR04040
STR04050
STR04060
STR04070
STR04080
STR04090
STR04100
STR04110
STR04120
STR04130
STR04140
STR04150
STR04160
STR04170
STR04180
STR04190
STR04200
STR04210
STR04220
STR04230
STR04240
STR04250
STR04260
STR04270
STR04280
STR04290
STR04300
STR04310

```













```

DO 4321 I = 1,NN
UVEL(I) = UVEL(I)/12.D0
VVFL(I) = VVFL(I)/12.D0
CONTINUE
DO 2345 I = 1,NN
UVEL(I)*12.D0
VVFL(I)*12.D0
CONTINUE
      COMPARE 'NEW STREAM FUNCTION' DISTRIBUTION WITH 'OLD
      STREAM FUNCTION DISTRIBUTION.
      X = 0.D0
DO 430 I = 1,NN
IF(PHI(I).EQ.0.D0)GOTO421
EPS = DABS((PSIO(I) - PSI(I))/PSI(I))
GOTO422
EPS = DABS(PSIO(I) - PSI(I))
IF (X.GT.EPS)GOTO430
X = EPS
CONTINUE
      ASK IF STREAM FUNCTION CONVERGENCE CRITERION BEEN SATISFIED?
      IF IT HAS.....WRITE RESULTS
      IF NOT.....ITERATE ONCE MORE.
      KK = KK + 1
      IF(X.LE.1.D-01)GOTO450
      WRITE (NWRITE,1400)KK,X
      FORMAT(' ',LARGEST FPS FOR ITERATION ',I2,' IS ',D19.12)
      IF (KK.LT.2)GOTO1500
      WRITE(NWRITE,1600)KK,X
      FORMAT(' ',PROGRAM TERMINATED ON ITERATION NO.',I3,/,',D19.12)
      1. RESULTS WHICH FOLLOW ARE FOR CONVERGENCE EPSILON = ',D19.12)
      GOTO1104
      1500 WRITE(NWRITE,1102)KK
      1102 FORMAT(' ',ITERATION NO.',I3,/,',COMPLETE',/,',STREAM FUNCTION CON
      IVERGENCE NOT YET SATISFIED.,/,',NEXT ITERATION IS IN PROGRESS',)
      NEXT ITERATION
      ZEROIZE STIFFNESS MATRIX AND RIGHT HAND SIDE VECTOR TO
      PREPARE FOR NEXT ITERATION.
      DO 460 I = 1,NN
      F(I) = 0.D0
      DO 460 J = 1,NN

```

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STR05290
STR05300
STR05310
STR05320
STR05330
STR05340
STR05350
STR05360
STR05370
STR05380
STR05390
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STR05410
STR05420
STR05430
STR05440
STR05450
STR05460
STR05470
STR05480
STR05490
STR05500
STR05510
STR05520
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STR05580
STR05590
STR05600
STR05610
STR05620
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STR05660
STR05670
STR05680
STR05690
STR05700
STR05710
STR05720
STR05730
STR05740
STR05750

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460      EM(I,J) = 0.00
      CONTINUE
C
C
C      REPLACE PSIO(I) WITH CURRENT VALUE OF PSI. RETURN
      TO 'CALL SLINE' STATEMENT AND RFCALCULATE BOTH THE
      STIFFNESS MATRIX AND RIGHT HANDRIGHT HAND
      SIDE VECTOR AND PERFORM NEW CALCULATION FOR PSI.
C
C
C      DO 470 I = 1,NN
      PSIO(I) = PSI(I)
      CONTINUE
C
C      NEXT ITERATION
C
C      GOTO1105
      WRITE(NWRITE,1200)KK
      FORMAT(' ',13,/, ' RESULTS ARE AS FOLLOWS.....')
      1 RATION NUMBER ' ,13,/, ' RESULTS ARE AS FOLLOWS.....')
      2 .....')
      WRITE OUT RESULTS
C
C      GOTO1111
C
C      CHANGE UNITS OF VELOCITY TO FT/SEC
C
C      DO 600 I = 1,NN
      UVEL(I) = UVEL(I)/12.00
      VVEL(I) = VVEL(I)/12.00
      TWEL(I) = TWEL(I)/12.00
      CCNTINUE
      WRITE(NWRITE,1110)
      FORMAT(' ',13,/, 'FINITE ELEMENT RESULTS',/,/, 'DENSITY',)
      1 ' NODE',5X,PSI(I),10X,VZ,13X,VR,12X,R(I),10X,DENSITY',)
      WRITE(NWRITE,1120)(I,PSI(I),UVEL(I),VVEL(I),RC(I),RHO(I),I=1,NN)
      FORMAT(' ',13,2X,D13.6,2X,D13.6,2X,D13.6,2X,D13.6)
      WRITE(NWRITE,1121)
      FORMAT(' ',13,2X,D13.6,2X,D13.6,2X,D13.6,2X,D13.6)
      WRITE(NWRITE,1300)(I,WRL(I),H(I),TWEL(I),I=1,NN)
      FORMAT(' ',13,2X,D13.6,2X,D13.6,2X,D13.6,2X,D13.6)
      STOP
      DEBUG SUBCHK
      END
      SUBROUTINE FCAL(F,W,H,ZA,EA,UVEL,RC,ZC,WRL,TVEL,NFS,NODE,NN,NE
      1,NFSP,TWEL,NTE)
      IMPLICIT REAL*8(A-H,P-Z)
      DIMENSION RJAC(2,2),F(107),W(9),D(8),E(8),SF(8),ZA(9),EA(9)
      DIMENSION UVEL(107),RC$(8),ZC$(8),RC(107),ZC(107),WRL(107)

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 STR05770  
 STR05780  
 STR05790  
 STR05800  
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 STR06160  
 STR06170  
 STR06180  
 STR06190  
 STR06200  
 STR06210  
 STR06220  
 STR06230



```

DIMENSION TVEL(107)
DIMENSION H(107),TWEL(107),F$(8),NFS(107),NODE(28,8),N(8),L1(2)
DIMENSION M1(2),NTE(40)
THIS SUBROUTINE CALCULATES THE RIGHT-HAND SIDE VECTOR
F(R,Z) FROM KNOWN RADIAL DISTRIBUTIONS OF WHIRL, ENTHALPY
, ROTHALPY, AND ENTROPY.
ZEROIZE OUT F$( ) .

DO 50 I = 1,8
F$(I) = 0.00
CONTINUE

CYCLE FOR EACH ELEMENT.

DO 100 II = 1,NE
RC$(1) = RC(NODE(II,1))
RC$(2) = RC(NODE(II,2))
RC$(3) = RC(NODE(II,3))
RC$(4) = RC(NODE(II,4))
RC$(5) = RC(NODE(II,5))
RC$(6) = RC(NODE(II,6))
RC$(7) = RC(NODE(II,7))
RC$(8) = RC(NODE(II,8))
ZC$(1) = ZC(NODE(II,1))
ZC$(2) = ZC(NODE(II,2))
ZC$(3) = ZC(NODE(II,3))
ZC$(4) = ZC(NODE(II,4))
ZC$(5) = ZC(NODE(II,5))
ZC$(6) = ZC(NODE(II,6))
ZC$(7) = ZC(NODE(II,7))
ZC$(8) = ZC(NODE(II,8))

CYCLE FOR EACH LOCAL NODE.

DO 200 I = 1,8
CHECK TO SEE IF PSI HAS BEEN SPECIFIED AT THE NODE.
IF SO ... DO NOT CALCULATE A VALUE OF F(R,Z) FOR THE
NODE TO AVOID OVER SPECIFICATION AND CYCLE FOR THE NEXT
NODE.

DO 210 L = 1,MNFS
LTEST = NODE(II,I) - NFS(L)
IF(LTEST.EQ.0)GOTO220
CONTINUE
GOTO200

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STR06620
STR06630
STR06640
STR06650
STR06660
STR06670
STR06680
STR06690
STR06700
STR06710

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```

C      CYCLE FOR EACH GAUSSIAN QUADRATURE INTEGRATION POINT.
C
C220  DO 300 J = 1,9
C      FIND THE APPROPRIATE SHAPE FUNCTIONS.
C      CALL SHAPE(EA(J),ZA(J),SF)
C      FIND THE JACOBIAN.
C      CALL JACOB(EA(J),ZA(J),D,E,RC$,ZC$,RJAC)
C      FIND THE DETERMINANT OF THE JACOBIAN.
C      DETJ = RJAC(1,1)*RJAC(2,2) - RJAC(1,2)*RJAC(2,1)
C      FIND THE INVERSE OF THE JACOBIAN.
C      CALL DMINV(RJAC,2,A,L1,M1)
C      FIND NI*UI,NI*V THETA I,NI*RI.....
C
C      SUMV = 0.D0
C      SUMV = 0.D0
C      SUMR = 0.D0
C      DO 110 KK = 1,8
C      SUMV = SUMV + SF(KK)*UVEL(NODE(II,KK))
C      IF(NTE(II).EQ.2)GOTO105
C      SUMV = SUMV + SF(KK)*TVEL(NODE(II,KK))
C      GOTO106
C      SUMV = SUMV + SF(KK)*TWEL(NODE(II,KK))
C      SUMR = SUMR + SF(KK)*RC(NODE(II,KK))
C      CONTINUE
C      FIND D(WHIRL)/DR
C
C      SUMW = 0.D0
C      DO 120 KK = 1,8
C      SUMW = SUMW + (RJAC(2,1)*D(KK) + RJAC(2,2)*E(KK))*WRL(NODE(II,KK))
C      CONTINUE
C
C      SUMH = 0.D0
C      DO 130 KK = 1,8
C      SUMH = SUMH - (RJAC(2,1)*D(KK) + RJAC(2,2)*E(KK))*H(NODE(II,KK))*
C      1 32.174D0*778.D0*144.D0
C
C105
C106
C110
C      C
C      C
C120
C      C
C      C
C121

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STR06720  
 STR06730  
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 STR07170  
 STR07180  
 STR07190





```

130      CONTINUE
C
C
C
131      FIND F$(NODE(II,I))
XX = SUMH + (SUMV/SUMR)*SUMW
XX = (SF(I)/SUMU)*XX*DETJ
F$(I) = F$(I) + XX*W(J)
CONTINUE
200 CONTINUE
C
C
C
ASSEMBLE RIGHT HAND SIDE VECTOR.
N(1) = NODE(II,1)
N(2) = NODE(II,2)
N(3) = NODE(II,3)
N(4) = NODE(II,4)
N(5) = NODE(II,5)
N(6) = NODE(II,6)
N(7) = NODE(II,7)
N(8) = NODE(II,8)
DO 400 I$ = 1,8
I = N(I$)
F(I) = F(I) + F$(I$)
CONTINUE
400
C
C
C
ZEROIZE OUT F$() FOR NEXT ELEMENTAL CALCULATION.
DO 500 I = 1,8
F$(I) = 0.00
CONTINUE
500
C
C
C
NEXT ELEMENT.
CONTINUE
RETURN
DERUG SUBCHK
END
SUBROUTINE JACOB(E1,Z1,D,E,RC$,ZC$,RJAC)
IMPLICIT REAL*(A-H,P-Z)
THIS SUBROUTINE CALCULATES THE JACOBIAN MATRIX FOR SUBSE
QUENT NUMERICAL INTEGRATIONS BY GAUSSIAN QUADRATURE.
DIMENSION RJAC(2,2),D(8),E(8),RC$(8),ZC$(8)
RJAC(1,1) = 0.00
RJAC(1,2) = 0.00
RJAC(2,1) = 0.00
RJAC(2,2) = 0.00
D(1) = (E1 + 2.00*Z1 + 2.00*Z1*E1 + E1*E1)/4.00

```



```

D(2) = -(Z1 + Z1*E1)
D(3) = (-E1 + 2.D0*Z1 + 2.D0*Z1*E1 - E1*E1)/4.D0
D(4) = (-1.D0 + F1*E1)/2.D0
D(5) = (E1 + 2.D0*Z1 - 2.D0*Z1*E1 - E1*E1)/4.D0
D(6) = -Z1 + Z1*E1
D(7) = (-E1 + 2.D0*Z1 - 2.D0*Z1*E1 + E1*E1)/4.D0
D(8) = (1.D0 - E1*E1)/2.D0
E(1) = (Z1 + 2.D0*E1 + Z1*Z1 + 2.D0*Z1*E1)/4.D0
E(2) = (1.D0 - Z1*Z1)/2.D0
E(3) = (-Z1 + 2.D0*E1 + Z1*Z1 - 2.D0*Z1*E1)/4.D0
E(4) = -E1 + E1*Z1
E(5) = (Z1 + 2.D0*E1 - Z1*Z1 - 2.D0*Z1*E1)/4.D0
E(6) = (-1.D0 + Z1*Z1)/2.D0
E(7) = (-Z1 + 2.D0*E1 - Z1*Z1 + 2.D0*Z1*E1)/4.D0
E(8) = -(E1 + Z1*E1)
DO 100 I = 1,8
  RJAC(1,1) = RJAC(1,1) + D(I)*ZC$(I)
  RJAC(1,2) = RJAC(1,2) + D(I)*RC$(I)
  RJAC(2,1) = RJAC(2,1) + E(I)*ZC$(I)
  RJAC(2,2) = RJAC(2,2) + E(I)*RC$(I)
CONTINUE
RETURN
DEBUG SUBCHK
END

```

100

```

SUBROUTINE VEL(NE,NN,RC,NODE,G,RG,TT,RHOT,RHON,ZC,PSI,RHO,B,UINLET
1,UVEL,VVEL,RHOSTA,ALP,BE,H,WG)

```

C C C C C C C C

```

THIS SUBROUTINE CALCULATES U AND V VELOCITIES AND A NEW
NODAL DENSITY FROM A KNOWN PSI DISTRIBUTION AT EACH OF
THE NODES IN THE SYSTEM. IN ADDITION, THE CALL STATEMENT
TRANSFERS THE NUMBER OF ELEMENTS, NODAL COORDINATES, LOCAL
NODE NUMBERS, RATIO OF SPECIFIC HEATS, GAS CONSTANT, TOTAL
TEMPERATURE, TOTAL DENSITY, THE LATEST CALCULATED NODAL
STREAM FUNCTION, DENSITY DISTRIBUTION, NODAL BLOCKAGE FAC-
TOR, AND INLET VELOCITY CONDITIONS.

```

```

IMPLICIT REAL*8(A-H,P-Z)
DIMENSION RJAC(2,2),PSI(107),D(8),E(8),UVEL(107),VVEL(107)
DIMENSION RC$(8),ZC$(8),RC(107),ZC(107),RHO(107),E1(8),Z1(8)
DIMENSION DR(8),DZ(8),B(107),RHON(107),H(107),ALP(107),BE(107)
DIMENSION NODE(28,8),L1(2)
DIMENSION M1(2)
DATA Z1/1.D0,0.D0,-1.D0,-1.D0,-1.D0,-1.D0,0.D0,1.D0,1.D0/
DATA E1/1.D0,1.D0,1.D0,0.D0,-1.D0,-1.D0,-1.D0,0.D0/
DO 100 I1 = 1,NE
  RC$(1) = RC(NODE(I1,1))
  RC$(2) = RC(NODE(I1,2))
  RC$(3) = RC(NODE(I1,3))
  RC$(4) = RC(NODE(I1,4))

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STR07680  
STR07690  
STR07700  
STR07710  
STR07720  
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STR07800  
STR07810  
STR07820  
STR07830  
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STR07850  
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STR08100  
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STR08120  
STR08130  
STR08140  
STR08150







```

301 IDEN = IDEN + 1
302 IF(NODE(II,I).LT.43)GOTO300
303 IF(NODE(II,I).GT.65)GOTO300
304 XM = (XL + XR)/2.D0
305 RI = RC(NODE(II,I))
306 BI = B(NODE(II,I))
307 WI = (PSIZ**2 + PSIR**2)/((XM*RI*BI)**2)
308 WI = (W1*144.D0*144.D0/32.174D0)/(DCOS(BETA)**2)
309 UI = (WG*RI)**2/(144.D0*32.174D0)
310 AI = (G - 1.D0)*(W1 - UI)/(2.D0*G*RG*TT)
311 A2 = DSQRT((PSIR**2+PSIZ**2)/((XM*RI*BI)**2))*DTAN(ALPHA)
312 A2 = (G - 1.D0)*(WG*RI)*A2/(G*RG*TT)
313 A2 = A2*12.D0/32.174D0
314 RHON(NODE(II,I)) = RHOT*((1.D0-A2-A1)**(1.D0/(G-1.D0)))
315 GOTO315
316 AI = (G - 1.D0)/(2.D0*G*RG*TT)
317 XM = (XL + XR)/2.D0
318 AI = AI/(XM)
319 AI = AI*144.D0*144.D0/32.174D0
320 AI = 1.D0 - AI*(PSIZ**2 + PSIR**2*(1.D0 + DTAN(ALPHA)**2))
321 AI = AI*(1.D0/(G - 1.D0))
322 RHON(NODE(II,I)) = RHOT*AI
323 EPS = RHON(NODE(II,I)) - XM
324 X4 = DABS(EPS)
325 IF(X4.LT.1.D-06)GOTO250
326 IF(IDEN.EQ.10)GOTO250
327 IF(EPS.LT.0.D0)GOTO310
328 XL = XM
329 GOTO301
330 XR = XM
331 GOTO301
332 IF(XM.GT.6.D-02)GOTO255
333 XM = 0.6D-01
334 RHON(NODE(II,I)) = XM
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C 500 DO 501 J = 3,5
502 VZ = UVEL(NODE(II,J))
STR09600
STR09610
STR09620
STR09630
STR09640
STR09650
STR09660
STR09670
STR09680
STR09690
STR09700
STR09710
STR09720
STR09730
STR09740
STR09750
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STR09780
STR09790
STR09800
STR09810
STR09820
STR09830
STR09840
STR09850
STR09860
STR09870
STR09880
STR09890
STR09900
STR09910
STR09920
STR09930
STR09940
STR09950
STR09960
STR09970
STR09980
STR09990
STR10000
STR10010
STR10020
STR10030
STR10040
STR10050
STR10060
STR10070

      A = BE(NODE(II,J))
      R = RC(NODE(II,J))
      H(NODE(II,J)) = (DSQRT(VZ*VZ+VR*VR)/DCOS(A))*2
      H(NODE(II,J)) = H(NODE(II,J))*2
      H(NODE(II,J)) = H(NODE(II,J))/7.209035D06 + HS(NODE(II,J))
      TWEL(NODE(II,J)) = DSQRT(VR*VR + VZ*VZ)*DTAN(A)
      WRL(NODE(II,J)) = R*(WG*R - TWEL(NODE(II,J)))
      CONTINUE
      GOTOL11

501
C
C
C 600      FIND H,WRL,AND TVEL AT LOC NNODES 3,4,5(STATOR).

      DO 601 J = 3,5
      VZ = UVEL(NODE(II,J))
      VR = VVEL(NODE(II,J))
      A = ALP(NODE(II,J))
      R = RC(NODE(II,J))
      H(NODE(II,J)) = (VR*VR+VZ*VZ)*(1.D0+DTAN(A))*2
      H(NODE(II,J)) = H(NODE(II,J))/7.209035D06 + HS(NODE(II,J))
      TVEL(NODE(II,J)) = DSQRT(VR*VR+VZ*VZ)*DTAN(A)
      WRL(NODE(II,J)) = R*TVEL(NODE(II,J))
      CONTINUE
      N = 2
      P = PSI(NODE(II,N))
      IT = 0
      I = II

      CHECK TO SEE IF P IS WITHIN THE PRESENT ELEMENT
      IF(P.GE.PSI(NODE(I,5)))GOTO140
      CHECK NEXT ELEMENT BELOW THE PRESENT ELEMENT.

      I = I + 1
      GOTOL30
      IF(P.GT.PSI(NODE(I,4)))GOTO170

140
      EL = EL(4)
      ER = EL(5)
      E = (EL + ER)/2.D0
      CALL SHAPE(E,-1.D0,SF)
      PA = SF(3)*PSI(NODE(I,3)) + SF(4)*PSI(NODE(I,4))
      I + SF(5)*PSI(NODE(I,5))
      CHECK FOR STREAMLINE CONVERGENCE
      EPS = DABS(PA - P)
      IF(EPS.LT.1.D-06)GOTO190
      IT = IT + 1
      IF(IT.GT.10)GOTO190
      IF(PA.LT.P)GOTO160

```



```

160 EL = E
    GOTOL150
170 ER = E
    GOTOL150
165 IF(P.GT.PSI(NODE(I,3)))GOTOL180
    EL = E1(3)
    ER = E1(4)
    GOTOL150
    CHECK NEXT ELEMENT ABOVE PRESENT ELEMENT
180 IF(KK.GT.0)GOTOL185
    IF(I.EQ.1)GOTOL165
    I = I - 1
    GOTOL140
185 IF(I.EQ.1.AND.N.EQ.2)GOTOL187
    IF(I.EQ.1.AND.N.EQ.8)GOTOL187
    I = I - 1
    GOTOL140
187 I = II
    GOTOL165
    CONVERGENCE CRITERIA SATISFIED.
    CHECK TO SEE WHAT TYPE OF ELEMENT.
    IF(NTE(II).EQ.3)GOTOL195
    IF(NTE(II).EQ.2)GOTOL196
    CALCULATE WHIRL AND STATIC ENTHALPY(DUCT)
    WRL(NODE(II,N)) = SF(3)*WRL(NODE(I,3)) + SF(4)*WRL(NODE(I,4))
    1 + SF(5)*WRL(NODE(I,5))
    HS(NODE(II,N)) = SF(3)*HS(NODE(I,3)) + SF(4)*HS(NODE(I,4))
    1 + SF(5)*HS(NODE(I,5))
    TVEL(NODE(II,N)) = WRL(NODE(II,N))/RC(NODE(II,N))
    CALCULATE TOT ENTHALPY AT THE NODE.
    H(NODE(II,N)) = UVEL(NODE(II,N))*2*(1.00 + DTAN(ALP(NODE(II,N))))*
    1*2)
    H(NODE(II,N)) = H(NODE(II,N)) + VVEL(NODE(II,N))*2
    H(NODE(II,N)) = HS(NODE(II,N)) + H(NODE(II,N))/7.20935006
    GOTOL199
    CALCULATE TOT ENTHALPY AT NODE(STATOR).
    H(NODE(II,N)) = SF(3)*H(NODE(I,3)) + SF(4)*H(NODE(I,4)) + SF(5)*
    1 H(NODE(I,5))
    CALCULATE TVEL,SWHIRL,AND STATIC ENTHALPY AT NODE(STATOR)
    VZ = UVEL(NODE(II,N))

```

STR10080  
 STR10090  
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 STR10310  
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 STR10380  
 STR10390  
 STR10400  
 STR10410  
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 STR10500  
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 STR10530  
 STR10540  
 STR10550



```
C
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C196
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C
C
VR = VVEL(NODE(II,N))
R = RC(NODE(II,N))
TWEL(NODE(II,N)) = DSQRT(VR*VR+VZ*VZ)*DTAN(ALP(NODE(II,N)))
WRL(NODE(II,N)) = R*TWEL(NODE(II,N))
HS(NODE(II,N)) = H(NODE(II,N)) - (VR*VR+VZ*VZ)*(1.D0+DTAN(ALP(
1 NODE(II,N))))**2)/7.209035D06
GOTO199
C
C
C
CALCULATE HREL AT NODE(ROTOR).
H(NODE(II,N)) = SF(3)*H(NODE(I,3)) + SF(4)*H(NODE(I,4)) +
1 SF(5)*H(NODE(I,5))
C
C
C
CALCULATE SWHIRL,TWEL,AND STATIC ENTHALPY AT NODE(ROTOR)
VZ = UVEL(NODE(II,N))
VR = VVEL(NODE(II,N))
R = RC(NODE(II,N))
TWEL(NODE(II,N)) = DSQRT(VR*VR+VZ*VZ)*DTAN(BE(NODE(II,N)))
WRL(NODE(II,N)) = R*(WG*R - TWEL(NODE(II,N)))
HS(NODE(II,N)) = H(NODE(II,N)) - (DSQRT(VR*VR+VZ*VZ)/DCOS(BE(NODE
1 (II,N))))**2/7.209035D06 +(WG*R)**2/7.209035D06
GOTO199
C
C199
IF(N.EQ.1)GOTO120
IF(N.GE.6)GOTO200
N = 6
GOTO115
N = N + 1
IF(N.GT.8)GOTO210
GOTO115
N = N - 8
GOTO115
GO TO NEXT ELEMENT.
CONTINUE
RETURN
DERUG SUBCHK
END
SUBROUTINE SHAPE(E,Z,SF)
IMPLICIT REAL*8(A-H,P-Z)
DIMENSION SF(8)
SF(1) = (Z*E + Z*Z + E*E + Z*Z*E + Z*E*E - 1.D0)/4.D0
SF(2) = (1.D0 + E - Z*Z - Z*Z*E)/2.D0
SF(3) = (-Z*E + Z*Z + E*E + Z*Z*E - Z*E*E - 1.D0)/4.D0
SF(4) = (1.D0 - E*E - Z + Z*E*E)/2.D0
SF(5) = (Z*E + Z*Z + E*E - Z*Z*E - Z*E*E - 1.D0)/4.D0
SF(6) = (1.D0 - E - Z*Z + E*Z*Z)/2.D0
SF(7) = (-Z*E + Z*Z + E*E - E*Z*Z + Z*E*E - 1.D0)/4.D0
```





SF(8) = (1.D0 - E*E + Z - Z*E*E)/2.D0				STR11040
RETURN				STR11050
DEBUG SUBCHK				STR11060
END				STR11070
				MPL000010
				MPL000040
				MPL000060
				MPL000090
				MPL000100
				MPL000110
				MPL000130
				MPL000140
				MPL000150
				MPL000180
				MPL000220
				MPL000260
				MPL000270
				MPL000280
				MPL000290
				MPL000340
				MPL000350
				MPL000360

```

SUBROUTINE MPLOT(RC,ZC,NODE,NN,NE)
  IMPLICIT REAL*8(A-H,P-Z)
  DIMENSION RC(NN),ZC(NN),OP1(9),OP2(9)
  DIMENSION O1(107),O2(107)
  DIMENSION NODE(NE,8)
  REAL*8 TITLE(3),GAVITO ,NASA ,TASK 1 ,/
  DATA OSCALE/.24/
  DO 100 L = 1,NN
    O1(L) = ZC(L)*NSCALE
    O2(L) = RC(L)*OSCALE
  CONTINUE
  CALL PLOTS
  CALL PLOT(0.0,3.0,-3)
  DO 200 I = 1,NE
    NPE = 9
    DO 300 J = 1,8
      OP1(J) = O1(NODE(I,J))
      OP2(J) = O2(NODE(I,J))
    CONTINUE
    CP1(NPE) = OP1(1)
    OP2(NPE) = OP2(1)
    CALL LINE(OP1,OP2,NPE,1,1)
  CONTINUE
  DO 400 K = 1,NN
    OL = FLOAT(K)
    CALL NUMBER(O1(K),O2(K),.07,OL,0,-1)
  CONTINUE
  CALL SYMBOL(0.0,5.0,-14,TITLE,0.0,24)
  CALL PLOT(0.0,7.0,-3)
  CALL PLOTE
  RETURN
  CEBUG SUBCHK
  END

```



# APPENDIX B SAMPLE INPUT DATA

NASA TASK-1	TRANSONIC	COMPRESSOR	
107	28		1.
1	0.0	18.878	1.
2	.00	17.439	1.
3	.00	16.0	1.
4	.00	14.5	1.
5	.00	13.0	1.
6	.00	11.5	1.
7	.00	10.0	1.
8	.00	8.5495	1.
9	0.	7.099	1.
10	3.	18.484	1.
11	3.	16.0	1.
12	3.	13.0	1.0
13	3.	10.0	1.
14	3.	7.099	1.
15	6.	18.409	1.
16	6.	17.205	1.0
17	6.0	16.0	1.
18	6.0	14.5	1.
19	6.0	13.0	1.
20	6.0	11.5	1.
21	6.0	10.0	1.
22	6.0	8.5495	1.
23	6.0	7.099	1.
24	8.902	18.403	1.
25	8.902	15.798	1.
26	8.902	12.897	1.
27	8.902	9.145	1.
28	8.902	7.147	1.
29	11.804	18.397	1.
30	11.804	16.596	1.
31	11.804	15.595	1.
32	11.804	14.194	1.
33	11.804	12.794	1.
34	11.804	11.393	1.
35	11.804	9.992	1.
36	11.804	8.591	1.
37	11.804	7.19	1.
38	15.5	18.37	1.
39	15.5	15.835	1.
40	15.5	13.3765	1.
41	15.5	10.23	1.
42	15.5	8.25	1.
43	18.447	18.161	.9921628
44	18.383	17.072	.991016
45	18.319	16.855	.989867
46	18.	14.	.988101



47	18.	256	13.	638	986334
48	18.	192	12.	659	984340
49	18.	128	11.	658	982346
50	18.	064	10.	403	978950
51	19.	524	9.	125	975553
52	19.	527	18.	037	954283
53	19.	528	16.	706	931421
54	19.	528	13.	778	896215
55	19.	53	11.	734	858371
56	20.	533	9.	631	792201
57	20.	599	17.	871	992424
58	20.	665	16.	937	991146
59	20.	731	16.	002	989867
60	20.	797	14.	888	988100
61	20.	862	13.	773	986336
62	20.	928	12.	875	984242
63	20.	928	11.	875	982148
64	20.	994	11.	009	989855
65	21.	06	10.	142	99755
66	21.	692	17.	838	1.
67	21.	802	15.	822	1.
68	21.	911	14.	286	1.
69	22.	031	12.	348	988014
70	22.	135	10.	836	987362
71	22.	85	17.	711	987650
72	22.	904	16.	586	986970
73	22.	958	15.	586	986091
74	22.	962	14.	132	985934
75	23.	028	14.	415	984777
76	23.	062	13.	415	983765
77	23.	096	12.	698	982754
78	23.	148	11.	625	902611
79	23.	225	10.	553	902895
80	24.	225	17.	836	904725
81	24.	615	15.	642	903892
82	24.	610	14.	228	902994
83	24.	605	12.	852	988014
84	24.	6	10.	831	987362
85	26.	436	17.	836	987650
86	26.	336	16.	767	986970
87	26.	273	15.	697	986091
88	26.	232	15.	011	98543
89	26.	191	14.	325	984777
90	26.	152	13.	665	983762
91	26.	113	12.	057	982754
92	26.	056	11.	057	1.
93	26.	0	11.	839	1.
94	29.	7	17.	839	1.



95	96	98	99	100	101	102	103	104	105	106	107	108	109	110	111	112	113	114	115	116	117	118	119	120	121	122	123	124	125	126	127	128	129	130	131	132	133	134	135	136	137	138	139	140	141	142	143	144	145	146	147	148	149	150	151	152	153	154	155	156	157	158	159	160	161	162	163	164	165	166	167	168	169	170	171	172	173	174	175	176	177	178	179	180	181	182	183	184	185	186	187	188	189	190	191	192	193	194	195	196	197	198	199	200	201	202	203	204	205	206	207	208	209	210	211	212	213	214	215	216	217	218	219	220	221	222	223	224	225	226	227	228	229	230	231	232	233	234	235	236	237	238	239	240	241	242	243	244	245	246	247	248	249	250	251	252	253	254	255	256	257	258	259	260	261	262	263	264	265	266	267	268	269	270	271	272	273	274	275	276	277	278	279	280	281	282	283	284	285	286	287	288	289	290	291	292	293	294	295	296	297	298	299	300	301	302	303	304	305	306	307	308	309	310	311	312	313	314	315	316	317	318	319	320	321	322	323	324	325	326	327	328	329	330	331	332	333	334	335	336	337	338	339	340	341	342	343	344	345	346	347	348	349	350	351	352	353	354	355	356	357	358	359	360	361	362	363	364	365	366	367	368	369	370	371	372	373	374	375	376	377	378	379	380	381	382	383	384	385	386	387	388	389	390	391	392	393	394	395	396	397	398	399	400	401	402	403	404	405	406	407	408	409	410	411	412	413	414	415	416	417	418	419	420	421	422	423	424	425	426	427	428	429	430	431	432	433	434	435	436	437	438	439	440	441	442	443	444	445	446	447	448	449	450	451	452	453	454	455	456	457	458	459	460	461	462	463	464	465	466	467	468	469	470	471	472	473	474	475	476	477	478	479	480	481	482	483	484	485	486	487	488	489	490	491	492	493	494	495	496	497	498	499	500	501	502	503	504	505	506	507	508	509	510	511	512	513	514	515	516	517	518	519	520	521	522	523	524	525	526	527	528	529	530	531	532	533	534	535	536	537	538	539	540	541	542	543	544	545	546	547	548	549	550	551	552	553	554	555	556	557	558	559	560	561	562	563	564	565	566	567	568	569	570	571	572	573	574	575	576	577	578	579	580	581	582	583	584	585	586	587	588	589	590	591	592	593	594	595	596	597	598	599	600	601	602	603	604	605	606	607	608	609	610	611	612	613	614	615	616	617	618	619	620	621	622	623	624	625	626	627	628	629	630	631	632	633	634	635	636	637	638	639	640	641	642	643	644	645	646	647	648	649	650	651	652	653	654	655	656	657	658	659	660	661	662	663	664	665	666	667	668	669	670	671	672	673	674	675	676	677	678	679	680	681	682	683	684	685	686	687	688	689	690	691	692	693	694	695	696	697	698	699	700	701	702	703	704	705	706	707	708	709	710	711	712	713	714	715	716	717	718	719	720	721	722	723	724	725	726	727	728	729	730	731	732	733	734	735	736	737	738	739	740	741	742	743	744	745	746	747	748	749	750	751	752	753	754	755	756	757	758	759	760	761	762	763	764	765	766	767	768	769	770	771	772	773	774	775	776	777	778	779	780	781	782	783	784	785	786	787	788	789	790	791	792	793	794	795	796	797	798	799	800	801	802	803	804	805	806	807	808	809	810	811	812	813	814	815	816	817	818	819	820	821	822	823	824	825	826	827	828	829	830	831	832	833	834	835	836	837	838	839	840	841	842	843	844	845	846	847	848	849	850	851	852	853	854	855	856	857	858	859	860	861	862	863	864	865	866	867	868	869	870	871	872	873	874	875	876	877	878	879	880	881	882	883	884	885	886	887	888	889	890	891	892	893	894	895	896	897	898	899	900	901	902	903	904	905	906	907	908	909	910	911	912	913	914	915	916	917	918	919	920	921	922	923	924	925	926	927	928	929	930	931	932	933	934	935	936	937	938	939	940	941	942	943	944	945	946	947	948	949	950	951	952	953	954	955	956	957	958	959	960	961	962	963	964	965	966	967	968	969	970	971	972	973	974	975	976	977	978	979	980	981	982	983	984	985	986	987	988	989	990	991	992	993	994	995	996	997	998	999	1000	1001	1002	1003	1004	1005	1006	1007	1008	1009	1010	1011	1012	1013	1014	1015	1016	1017	1018	1019	1020	1021	1022	1023	1024	1025	1026	1027	1028	1029	1030	1031	1032	1033	1034	1035	1036	1037	1038	1039	1040	1041	1042	1043	1044	1045	1046	1047	1048	1049	1050	1051	1052	1053	1054	1055	1056	1057	1058	1059	1060	1061	1062	1063	1064	1065	1066	1067	1068	1069	1070	1071	1072	1073	1074	1075	1076	1077	1078	1079	1080	1081	1082	1083	1084	1085	1086	1087	1088	1089	1090	1091	1092	1093	1094	1095	1096	1097	1098	1099	1100	1101	1102	1103	1104	1105	1106	1107	1108	1109	1110	1111	1112	1113	1114	1115	1116	1117	1118	1119	1120	1121	1122	1123	1124	1125	1126	1127	1128	1129	1130	1131	1132	1133	1134	1135	1136	1137	1138	1139	1140	1141	1142	1143	1144	1145	1146	1147	1148	1149	1150	1151	1152	1153	1154	1155	1156	1157	1158	1159	1160	1161	1162	1163	1164	1165	1166	1167	1168	1169	1170	1171	1172	1173	1174	1175	1176	1177	1178	1179	1180	1181	1182	1183	1184	1185	1186	1187	1188	1189	1190	1191	1192	1193	1194	1195	1196	1197	1198	1199	1200	1201	1202	1203	1204	1205	1206	1207	1208	1209	1210	1211	1212	1213	1214	1215	1216	1217	1218	1219	1220	1221	1222	1223	1224	1225	1226	1227	1228	1229	1230	1231	1232	1233	1234	1235	1236	1237	1238	1239	1240	1241	1242	1243	1244	1245	1246	1247	1248	1249	1250	1251	1252	1253	1254	1255	1256	1257	1258	1259	1260	1261	1262	1263	1264	1265	1266	1267	1268	1269	1270	1271	1272	1273	1274	1275	1276	127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70 .871967  
 71 .692198  
 72 .672301  
 73 .652404  
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 76 .740544  
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 78 .810444  
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43 1.08  
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 52 1.040565  
 53 .967785  
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 55 .707731  
 56 .477173  
 57 1.001121  
 58 .971145  
 59 .941605  
 60 .848405  
 61 .755204  
 62 .657117  
 63 .559029  
 64 .361283  
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43	17	.	1250719
52	17	.	1250719
57	17	.	1250719
66	17	.	1250719
71	17	.	1250719
80	17	.	1250719
85	17	.	1250719
94	17	.	1250719
14		0	0
23		0	0
38		0	0
57		0	0
72		0	0
81		0	0
95		0	0
55		0	0
70		0	0
79		0	0
84		0	0
93		0	0
98		0	0
1	1	2	3
1	1	3	6
1	1	6	7
1	1	8	9
1	2	0	1
2	2	2	5
2	2	5	6
2	2	6	7
3	3	0	1
3	3	3	2
3	3	3	3
3	3	4	5
3	3	5	6
3	3	6	9
4	4	0	1
4	4	1	4
4	4	4	5

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# APPENDIX C SAMPLE OUTPUT LISTING

NASA TASK-1 TRANSONIC COMPRESSOR									
NO. OF NODES = 107									
NO. OF ELEMENTS = 28									
SUMMARY OF NODAL COORDINATES									
NODE	Z(I)	R(I)	ANG(I)	B(I)	REL FLOW ANG	ABS FLOW ANG	REL FLOW ANG	ABS FLOW ANG	REL FLOW ANG
1	0.0	0.188780D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
2	0.0	0.174390D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
3	0.0	0.160000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
4	0.0	0.145000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
5	0.0	0.130000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
6	0.0	0.115000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
7	0.0	0.100000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
8	0.0	0.854950D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
9	0.0	0.709900D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
10	0.300000D	0.184840D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
11	0.300000D	0.160000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
12	0.300000D	0.130000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
13	0.300000D	0.100000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
14	0.300000D	0.709900D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
15	0.600000D	0.184090D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
16	0.600000D	0.172050D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
17	0.600000D	0.160000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
18	0.600000D	0.145000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
19	0.600000D	0.130000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
20	0.600000D	0.115000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
21	0.600000D	0.854950D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
22	0.600000D	0.709900D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
23	0.600000D	0.184030D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
24	0.890200D	0.157980D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
25	0.890200D	0.128970D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
26	0.890200D	0.999600D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
27	0.890200D	0.714500D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
28	0.118040D	0.183970D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
29	0.118040D	0.169960D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
30	0.118040D	0.155950D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
31	0.118040D	0.141940D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
32	0.118040D	0.127940D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
33	0.118040D	0.113930D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
34	0.118040D	0.999200D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
35	0.118040D	0.859100D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
36	0.118040D	0.719000D	01	0.100000D	0.0	0.0	0.0	0.0	0.0
37	0.155000D	0.183700D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
38	0.155000D	0.158350D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
39	0.155000D	0.133000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
40	0.155000D	0.107650D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
41	0.155000D	0.823000D	02	0.100000D	0.0	0.0	0.0	0.0	0.0
42	0.155000D	0.823000D	01	0.100000D	0.0	0.0	0.0	0.0	0.0



43 0.1851100 02 0.1825000 02 0.9921630 00 0.7555530 00 0.1080000 01  
44 0.1844700 02 0.1716100 02 0.9910160 00 0.7553790 00 0.1036900 01  
45 0.1838300 02 0.1607200 02 0.9898670 00 0.7550290 00 0.9937910 01  
46 0.1831900 02 0.1485500 02 0.9881010 00 0.7216940 00 0.9506810 00  
47 0.1825600 02 0.1363800 02 0.9863340 00 0.6881830 00 0.9075710 00  
48 0.1819200 02 0.1265900 02 0.9843400 00 0.6314600 00 0.8819150 00  
49 0.1812800 02 0.1168000 02 0.9823460 00 0.5747370 00 0.8562590 00  
50 0.1806400 02 0.1040300 02 0.9789500 00 0.4757770 00 0.8235340 00  
51 0.1800000 02 0.9125000 01 0.9755530 00 0.3768170 00 0.7908090 00  
52 0.1952200 02 0.1801000 02 0.9542830 00 0.7237780 00 0.1040570 01  
53 0.1952700 02 0.1603700 02 0.9314210 00 0.7037170 00 0.9677850 00  
54 0.1952700 02 0.1370600 02 0.8962150 00 0.7101750 00 0.8314750 00  
55 0.1952800 02 0.1177800 02 0.8583710 00 0.6700030 00 0.7077310 00  
56 0.1953300 02 0.9634000 01 0.7922010 00 0.6244790 00 0.4771730 00  
57 0.2053900 02 0.1787100 02 0.9924240 00 0.6921980 00 0.1001120 01  
58 0.2059300 02 0.1693700 02 0.9911450 00 0.6723010 00 0.9714500 00  
59 0.2066500 02 0.1600200 02 0.9898670 00 0.6522400 00 0.9416050 00  
60 0.2073100 02 0.1488800 02 0.9881000 00 0.6923720 00 0.8484050 00  
61 0.2079700 02 0.1377300 02 0.9863360 00 0.7321660 00 0.7552040 00  
62 0.2086200 02 0.1282400 02 0.9842420 00 0.7489210 00 0.6571170 00  
63 0.2092800 02 0.1187500 02 0.9821480 00 0.7655010 00 0.5590290 00  
64 0.2099400 02 0.1100900 02 0.9898520 00 0.8710940 00 0.3612830 00  
65 0.2106000 02 0.1014200 02 0.9975550 00 0.8719660 00 0.1635370 00  
66 0.2169200 02 0.1783800 02 0.1000000 01 0.6921980 00 0.0 0  
67 0.2180200 02 0.1582200 02 0.1000000 01 0.6522400 00 0.0 0  
68 0.2191100 02 0.1400000 02 0.1000000 01 0.7321660 00 0.0 0  
69 0.2203100 02 0.1228600 02 0.1000000 01 0.7572100 00 0.0 0  
70 0.2213000 02 0.1034800 02 0.1000000 01 0.8719670 00 0.0 0  
71 0.2285000 02 0.1783600 02 0.9880140 00 0.6921980 00 0.0 0  
72 0.2290400 02 0.1671100 02 0.9873620 00 0.6723010 00 0.0 0  
73 0.2295800 02 0.1558600 02 0.9876500 00 0.6522400 00 0.0 0  
74 0.2302800 02 0.1485900 02 0.9869700 00 0.6923720 00 0.0 0  
75 0.2306200 02 0.1413200 02 0.9860910 00 0.7321660 00 0.0 0  
76 0.2309600 02 0.1341500 02 0.9859340 00 0.7405440 00 0.0 0  
77 0.2314800 02 0.1269800 02 0.9847770 00 0.7489210 00 0.0 0  
78 0.2320000 02 0.1162500 02 0.9837650 00 0.8104440 00 0.0 0  
79 0.2462500 02 0.1783600 02 0.9827540 00 0.8719670 00 0.0 0  
80 0.2461500 02 0.1564200 02 0.9026110 00 0.3460990 00 0.0 0  
81 0.2461000 02 0.1422800 02 0.9047250 00 0.3262020 00 0.0 0  
82 0.2460500 02 0.1285200 02 0.9038920 00 0.3661700 00 0.0 0  
83 0.2460000 02 0.1083100 02 0.9029940 00 0.4030000 00 0.0 0  
84 0.2633600 02 0.1783600 02 0.9880140 00 0.0 0.0 0.0 0  
85 0.2637300 02 0.1676700 02 0.9873620 00 0.0 0.0 0.0 0  
86 0.2623200 02 0.1569700 02 0.9876500 00 0.0 0.0 0.0 0  
87 0.2619100 02 0.1501100 02 0.9869700 00 0.0 0.0 0.0 0  
88 0.2615200 02 0.1432500 02 0.9860910 00 0.0 0.0 0.0 0  
89 0.2615200 02 0.1366500 02 0.9854300 00 0.0 0.0 0.0 0  
90 0.2615200 02 0.1366500 02 0.9854300 00 0.0 0.0 0.0 0







INLET THERMODYNAMIC VARIABLES ARE AS FOLLOWS

FLOW RATE = 0.107600D 03 LBM/SEC  
TOT DENSITY = 0.819200D-01 LBM CU FT  
TOT PRESSURE = 0.150546 D 02 PSI  
TOT TEMPERATURE = 0.499380D 03 DEG RANKINE  
ROTATIONAL SPEED = 0.435950D 04 RPM  
INLET U VELOCITY = 0.201483D 03 FT/SEC  
OUTLET U VELOCITY = 0.318847D 03 FT/SEC  
GAS CONSTANT = 0.533500D 02  
RATIO OF SPECIFIC HEATS = 0.140000D 01  
SPECIFIC HEAT AT CONSTANT PRESSURE = 0.240000D 00  
STATIC DENSITY AT INLET = 0.800000D-01  
INITIAL ESTIMATE OF PSI DISTRIBUTION = 0.171251D 02  
NODES WHERE PSI IS SPECIFIED

NODE NO.	PSI(I)
10	0.171251D 02
15	0.171251D 02
24	0.171251D 02
29	0.171251D 02
38	0.171251D 02
43	0.171251D 02
52	0.171251D 02
57	0.171251D 02
66	0.171251D 02
71	0.171251D 02
80	0.171251D 02
85	0.171251D 02
94	0.171251D 02
14	0.0
23	0.0
28	0.0
37	0.0
42	0.0
51	0.0
56	0.0





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65 0.0
70 0.0
79 0.0
84 0.0
93 0.0
98 0.0
1 0.171251D 02
2 0.142002D 02
3 0.115071D 02
4 0.894662D 01
5 0.663797D 01
6 0.458117D 01
7 0.277622D 01
8 0.127036D 01
9 0.0
99 0.171251D 02
100 0.145999D 02
101 0.121933D 02
102 0.981814D 01
103 0.757093D 01
104 0.545171D 01
105 0.346047D 01
106 0.167140D 01
107 0.0
NODES WHERE F(R,Z) IS SPECIFIED

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NODE NO.
11 12 13 16 17 18 19 20 21
22 25 26 27 30 31 32 33 34
35 36 39 40 41 44 45 46 47
48 49 50 53 54 55 58 59 60
61 62 63 64 67 68 69 72 73
74 75 76 77 78 81 82 83 86
87 88 89 90 91 92 95 96 97

LARGEST EPS FOR ITERATION 1 IS 0.136047897529D 02
ITERATION NO. 1 COMPLETE
STREAM FUNCTION CONVERGENCE NOT YET SATISFIED.
NEXT ITERATION IS IN PROGRESS
LARGEST EPS FOR ITERATION 2 IS 0.442913378700D 00
PROGRAM TERMINATED ON ITERATION NO. 2
RESULTS WHICH FOLLOW ARE FOR CONVERGENCE EPSILON = 0.442913378700D 00

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# FINITE ELEMENT RESULTS



NODE	PSI(I)	VZ	VR	R(I)	DENSITY
1	0.171251D 02	0.201483D 03	0.0	0.188780D 02	0.800000D-01
2	0.142002D 02	0.201483D 03	0.0	0.174390D 02	0.800000D-01
3	0.115071D 01	0.201483D 03	0.0	0.160000D 02	0.800000D-01
4	0.894662D 01	0.201483D 03	0.0	0.145000D 02	0.800000D-01
5	0.663797D 01	0.201483D 03	0.0	0.130000D 02	0.800000D-01
6	0.458117D 01	0.201483D 03	0.0	0.115000D 02	0.800000D-01
7	0.277622D 01	0.201483D 03	0.0	0.100000D 02	0.800000D-01
8	0.127036D 01	0.201483D 03	0.0	0.854950D 01	0.800000D-01
9	0.0	0.201483D 03	0.0	0.709900D 01	0.800000D-01
10	0.171251D 02	0.220059D 03	-0.172013D 02	0.184840D 02	0.802734D-01
11	0.118445D 02	0.210036D 03	-0.114073D 02	0.160000D 02	0.804297D-01
12	0.678256D 01	0.206122D 03	-0.730155D 01	0.130000D 02	0.804687D-01
13	0.282503D 01	0.202621D 03	-0.272330D 01	0.100000D 02	0.805078D-01
14	0.0	0.205347D 03	0.0	0.709900D 01	0.804883D-01
15	0.171251D 02	0.211902D 03	-0.38116D 00	0.184090D 02	0.803906D-01
16	0.145630D 02	0.216573D 03	-0.465115D 01	0.172050D 02	0.803125D-01
17	0.121188D 02	0.216545D 03	-0.158781D 01	0.160000D 02	0.803125D-01
18	0.937887D 01	0.212585D 03	-0.679883D 01	0.145000D 02	0.803906D-01
19	0.695622D 01	0.213867D 03	-0.684264D 01	0.130000D 02	0.803516D-01
20	0.477052D 01	0.212284D 03	-0.673067D 01	0.115000D 02	0.803906D-01
21	0.286757D 01	0.204643D 03	-0.564721D 01	0.100000D 02	0.805078D-01
22	0.132090D 01	0.206900D 03	0.225277D 01	0.854950D 01	0.804687D-01
23	0.0	0.210041D 03	0.336558D 01	0.709900D 01	0.804297D-01
24	0.171251D 02	0.227675D 03	-0.470728D 00	0.184030D 02	0.801562D-01
25	0.119735D 02	0.205688D 03	-0.166029D 02	0.157980D 02	0.804687D-01
26	0.702133D 01	0.220263D 03	-0.148156D 02	0.128970D 02	0.802539D-01
27	0.292664D 01	0.226396D 03	-0.223632D 01	0.999600D 01	0.801953D-01
28	0.0	0.198306D 03	0.310921D 01	0.714500D 01	0.805664D-01
29	0.171251D 02	0.226429D 03	0.109332D 01	0.183970D 02	0.801758D-01
30	0.142776D 02	0.183610D 03	0.795651D 02	0.169960D 02	0.805469D-01
31	0.122341D 02	0.206530D 03	-0.166455D 03	0.155950D 02	0.795312D-01
32	0.974105D 01	0.228187D 03	-0.172725D 03	0.141940D 02	0.791406D-01
33	0.724815D 01	0.241888D 03	-0.179660D 03	0.127940D 02	0.788672D-01
34	0.498124D 01	0.245654D 03	-0.130826D 03	0.113930D 02	0.792969D-01
35	0.292974D 01	0.245873D 03	-0.662508D 02	0.999200D 01	0.792666D-01
36	0.124448D 01	0.218274D 03	-0.183315D 02	0.859100D 01	0.802930D-01
37	0.0	0.181316D 03	0.469758D 02	0.719000D 01	0.807422D-01
38	0.171251D 02	0.953714D 02	-0.209029D 01	0.183700D 02	0.816016D-01
39	0.156118D 02	0.211283D 03	0.488500D-01	0.158350D 02	0.803906D-01
40	0.107447D 02	0.341329D 03	0.124478D 02	0.133000D 02	0.780078D-01
41	0.467601D 01	0.359152D 03	0.419968D 02	0.107650D 02	0.775391D-01
42	0.0	0.365127D 03	0.114029D 03	0.823000D 01	0.770312D-01
43	0.171251D 02	0.188915D 03	-0.542827D 02	0.182500D 02	0.836719D-01
44	0.150238D 02	0.182983D 03	-0.363786D 02	0.171610D 02	0.840625D-01
45	0.131222D 02	0.181377D 03	-0.358019D 02	0.160720D 02	0.835156D-01



46	0.109989D	02	0.217508D	03	-0.332291D	02	0.148550D	02	0.804687D-01
47	0.874510D	01	0.263002D	03	-0.321793D	02	0.1326380D	02	0.771484D-01
48	0.684972D	01	0.300928D	03	-0.128776D	02	0.126590D	02	0.751172D-01
49	0.490441D	01	0.357638D	03	-0.801256D	01	0.116800D	02	0.718555D-01
50	0.237289D	01	0.385140D	03	0.629724D	02	0.104030D	02	0.710547D-01
51	0.0	01	0.433195D	03	0.144257D	03	0.912500D	01	0.681250D-01
52	0.171251D	02	0.242434D	03	-0.54414D	02	0.180100D	02	0.800000D-01
53	0.132234D	02	0.208945D	03	0.543975D	01	0.160370D	02	0.826172D-01
54	0.883947D	01	0.334585D	03	0.477602D	02	0.137060D	02	0.726172D-01
55	0.476760D	01	0.538251D	03	0.107145D	03	0.117780D	02	0.600391D-01
56	0.0	01	0.684311D	03	0.227433D	03	0.963400D	01	0.600391D-01
57	0.171251D	02	0.281327D	03	-0.117674D	02	0.178710D	02	0.800000D-01
58	0.147764D	02	0.236773D	03	0.134070D	02	0.169370D	02	0.817578D-01
59	0.128904D	02	0.217194D	03	0.529913D	02	0.160020D	02	0.825391D-01
60	0.106224D	02	0.252037D	03	0.812320D	02	0.148880D	02	0.789453D-01
61	0.827315D	01	0.303197D	03	0.114025D	03	0.137730D	02	0.743359D-01
62	0.619073D	01	0.341721D	03	0.132514D	03	0.128240D	02	0.717969D-01
63	0.408225D	01	0.401864D	03	0.150547D	03	0.118750D	02	0.681836D-01
64	0.207387D	01	0.491840D	03	0.147459D	03	0.110090D	02	0.618750D-01
65	0.0	01	0.567354D	03	-0.109494D	03	0.101420D	02	0.600391D-01
66	0.171251D	02	0.302506D	03	0.456957D	01	0.178380D	02	0.767383D-01
67	0.120681D	02	0.255341D	03	0.349385D	02	0.158220D	02	0.783984D-01
68	0.798850D	01	0.300666D	03	0.802308D	02	0.140000D	02	0.762500D-01
69	0.417127D	01	0.334517D	03	0.980101D	02	0.122860D	02	0.745703D-01
70	0.0	01	0.445955D	03	0.856484D	02	0.103480D	02	0.662695D-01
71	0.171251D	02	0.301848D	03	0.307300D	-12	0.178360D	02	0.767578D-01
72	0.140702D	02	0.292879D	03	0.105376D	02	0.167110D	02	0.772070D-01
73	0.112853D	02	0.299853D	03	0.288777D	02	0.155860D	02	0.771094D-01
74	0.950536D	01	0.310703D	03	0.432739D	02	0.148590D	02	0.764062D-01
75	0.774640D	01	0.328817D	03	0.559861D	02	0.141320D	02	0.753125D-01
76	0.606420D	01	0.326266D	03	0.632255D	02	0.134150D	02	0.752734D-01
77	0.448194D	01	0.328199D	03	0.724202D	02	0.126980D	02	0.750781D-01
78	0.220067D	01	0.357466D	03	0.758258D	02	0.116250D	02	0.728516D-01
79	0.0	01	0.401487D	03	0.797238D	02	0.105530D	02	0.690625D-01
80	0.171251D	02	0.338282D	03	0.0	02	0.178360D	02	0.775781D-01
81	0.110657D	02	0.357678D	03	0.267016D	02	0.156420D	02	0.771094D-01
82	0.742061D	01	0.358663D	03	0.434724D	02	0.142280D	02	0.769141D-01
83	0.420615D	01	0.347499D	03	0.534363D	02	0.128520D	02	0.770312D-01
84	0.0	01	0.390797D	03	0.776011D	02	0.108310D	02	0.755273D-01
85	0.171251D	02	0.312169D	03	0.567579D	00	0.178360D	02	0.786328D-01
86	0.139682D	02	0.316128D	03	-0.126945D	03	0.167670D	02	0.780078D-01
87	0.109162D	02	0.335360D	03	-0.277874D	03	0.156970D	02	0.755859D-01
88	0.902395D	01	0.324992D	03	-0.331898D	03	0.150110D	02	0.747656D-01
89	0.727694D	01	0.322973D	03	-0.392978D	03	0.143250D	02	0.733594D-01
90	0.567134D	01	0.320579D	03	-0.356204D	03	0.136650D	02	0.743164D-01
91	0.414305D	01	0.319875D	03	-0.318186D	03	0.130050D	02	0.751562D-01
92	0.203268D	01	0.333436D	03	-0.163312D	03	0.120570D	02	0.773047D-01
93	0.0	01	0.357598D	03	-0.321838D	01	0.111090D	02	0.776172D-01



94	0.171251D	02	0.101387D	03	0.137034D-06	0.178390D	02	0.815625D-01
95	0.154134D	02	0.250834D	03	-0.272363D 01	0.159490D	02	0.798047D-01
96	0.122799D	02	0.434998D	03	-0.547570D 01	0.144130D	02	0.756250D-01
97	0.750549D	01	0.718042D	03	-0.510535D 01	0.129000D	02	0.680078D-01
98	0.0		0.806328D	03	-0.702657D 01	0.11400D	02	0.666016D-01
99	0.171251D	02	0.325522D	03	-0.591858D 00	0.178360D	02	0.783594D-01
100	0.145999D	02	0.328140D	03	0.128272D 03	0.170180D	02	0.777344D-01
101	0.121933D	02	0.337292D	03	0.274692D 03	0.162000D	02	0.756250D-01
102	0.981814D	01	0.342601D	03	0.328501D 03	0.153500D	02	0.744531D-01
103	0.757093D	01	0.350509D	03	0.393343D 03	0.145000D	02	0.727734D-01
104	0.545171D	01	0.346510D	03	0.362038D 03	0.136500D	02	0.736133D-01
105	0.346047D	01	0.342781D	03	0.329248D 03	0.128000D	02	0.744141D-01
106	0.167140D	01	0.329964D	03	0.170334D 03	0.119850D	02	0.773047D-01
107	0.0		0.325522D	03	0.274369D 01	0.111700D	02	0.783594D-01
NODE	WRL ( I )		HT		VT			
1	0.0		119851D	03	0.0	0.0		
2	0.0		119851D	03	0.0	0.0		
3	0.0		119851D	03	0.0	0.0		
4	0.0		119851D	03	0.0	0.0		
5	0.0		119851D	03	0.0	0.0		
6	0.0		119851D	03	0.0	0.0		
7	0.0		119851D	03	0.0	0.0		
8	0.0		119851D	03	0.0	0.0		
9	0.0		120023D	03	0.0	0.0		
10	0.0		119931D	03	0.0	0.0		
11	0.0		119892D	03	0.0	0.0		
12	0.0		119866D	03	0.0	0.0		
13	0.0		119882D	03	0.0	0.0		
14	0.0		119997D	03	0.0	0.0		
15	0.0		119983D	03	0.0	0.0		
16	0.0		119979D	03	0.0	0.0		
17	0.0		119955D	03	0.0	0.0		
18	0.0		119935D	03	0.0	0.0		
19	0.0		119925D	03	0.0	0.0		
20	0.0		119876D	03	0.0	0.0		
21	0.0		119885D	03	0.0	0.0		
22	0.0		119901D	03	0.0	0.0		
23	0.0		120006D	03	0.0	0.0		
24	0.0		119972D	03	0.0	0.0		
25	0.0		119963D	03	0.0	0.0		
26	0.0		119961D	03	0.0	0.0		
27	0.0		119825D	03	0.0	0.0		
28	0.0		120010D	03	0.0	0.0		
29	0.0		119956D	03	0.0	0.0		
30	0.0		119990D	03	0.0	0.0		
31	0.0		119990D	03	0.0	0.0		
32	0.0		120003D	03	0.0	0.0		
33	0.0		120028D	03	0.0	0.0		





[illegible]



82	0.244303D	05	0.143088D	03	0.0
83	0.265507D	05	0.172157D	03	0.0
84	0.326492D	05	0.251202D	03	0.0
85	0.0		0.0		0.0
86	0.0		0.0		0.0
87	0.0		0.0		0.0
88	0.0		0.0		0.0
89	0.0		0.0		0.0
90	0.0		0.0		0.0
91	0.0		0.0		0.0
92	0.0		0.0		0.0
93	0.0		0.0		0.0
94	0.0		0.0		0.0
95	0.0		0.0		0.0
96	0.0		0.0		0.0
97	0.0		0.0		0.0
98	0.0		0.0		0.0
99	0.0		0.0		0.0
100	0.0		0.0		0.0
101	0.0		0.0		0.0
102	0.0		0.0		0.0
103	0.0		0.0		0.0
104	0.0		0.0		0.0
105	0.0		0.0		0.0
106	0.0		0.0		0.0
107	0.0		0.0		0.0

0.124673D	03	0.0
0.127365D	03	0.0
0.134132D	03	0.0
0.119987D	03	0.0
0.120783D	03	0.0
0.122067D	03	0.0
0.123223D	03	0.0
0.124821D	03	0.0
0.126075D	03	0.0
0.127436D	03	0.0
0.130339D	03	0.0
0.134132D	03	0.0
0.120279D	03	0.0
0.122120D	03	0.0
0.125018D	03	0.0
0.127731D	03	0.0
0.132648D	03	0.0
0.120854D	03	0.0
0.121376D	03	0.0
0.122195D	03	0.0
0.123484D	03	0.0
0.125192D	03	0.0
0.126543D	03	0.0
0.128131D	03	0.0
0.129812D	03	0.0
0.131572D	03	0.0



## APPENDIX D

### CALCULATION OF ROTOR ELEMENT FLOW ANGLES

The following is a brief synopsis of the procedure contained in Ref.13 for calculating the outlet relative flow angles in a rotor element from the given inlet relative flow angle and blade solidity. The reader is referred to Ref.13, Chapter VI, for specific details of low speed correlation data.

As stated in Section III.A, uniform flow conditions at the rotor blade edges were assumed. This assumption coupled with knowledge of the mass flow rate and rotational speed, enables one to calculate the inlet relative flow angle,  $\beta_1$ , as shown in Fig 18.

From blade geometry information, the blade solidity,  $\sigma$ ,

$$\sigma = \frac{c}{s} \quad (1)$$

is obtained. At this point,  $\beta_1$ , and  $\sigma$  are given and one may calculate  $\beta_2$ , the rotor outlet relative flow angle from correlation curves depicted in Ref 13. The equation used to determine  $\beta_2$ , is the following,

$$\beta_2 = K_2 + \delta \quad (2)$$

where  $K_2$  is the angle between the tangent to the blade mean



camber line and the axial direction (Fig 18) . This is obtained from the blade geometry data.  $\delta$  is the low speed deviation angle which is obtained from the correlation curves in Ref. 13. The following equations show the relationship between  $\delta$  and the correlation data.

$$\delta = \delta_o^\circ + m\phi \quad (3)$$

$$\delta_o^\circ = (K\delta)_{sh} (K\delta)_t (\delta_o)_{io} \quad (4)$$

The variables  $m, (K\delta)_{sh}, (K\delta)_t$  and  $(\delta_o)_{io}$  , are all values which are obtained from the correlation curves and are all functions of the given blade geometry. The quantity,  $\phi$  , is the blade camber angle and again is obtained from the blade geometry data. Once all the variables are obtained from the correlation data, equation (4) is solved for the deviation angle for an uncambered blade section,  $\delta_o$  , and then equation (3) is solved for the deviation angle,  $\delta$  . One now calculates  $\beta_2$  from equation (2) for the blade element. With  $\beta_2$  now a known quantity, one now calculates the absolute flow angle,  $\alpha_2$  , from uniform flow assumptions.

An example follows for node numbers 43 and 57 (Fig 6) . From Ref. [12], Table II, the following quantities are obtained assuming the angle of incidence,  $i$  , (Fig 18) is zero and therefore the inlet relative flow angle,  $\beta_1$  , is equal to  $k_1$  .

$$\beta_1 = k_1 = 61.88^\circ$$

$$r = 1.3062$$

$$\phi = 6.95^\circ$$





$$K_2 = 54.93^\circ$$

$$\frac{t}{c})_{\max} = 0.035$$

$$\text{tip radius} = 18.25 \text{ in}$$

$$\text{hub radius} = 9.125 \text{ in}$$

Assuming uniform flow at the rotor inlet and a rotational speed of 4359.5 RPM, the following quantities are determined from the rotor inlet velocity diagram (Fig 18).

$$V_m = \frac{\dot{m}}{\rho A} = \frac{(107.6 \text{ lbm/sec})(144 \text{ in}^2/\text{ft}^2)}{(0.08 \text{ lbm/ft}^3) \pi (18.25^2 - 9.125^2) \text{ in}^2}$$

$$V_m = 246.802 \text{ Ft/sec}$$

where the area A, is determined from the hub and tip radii and the density is assumed to be 0.08 lbm/cu ft.

Now one is ready to obtain the correlation data. From Ref.[13], Fig 162, with  $\beta_1 = 61.88^\circ$  and  $\Gamma = 1.3062$ ,

$$\delta_o)_{\delta} = 2.50^\circ$$

From Ref.[13], Fig 162, with  $\beta_1 = 61.88^\circ$  and  $\Gamma = 1.3062$ ,

$$m = 0.235$$

From Ref.[13], Fig 172, with  $t/c)_{\max} = 0.0350$ ,

$$K\delta)t = 0.29$$

From Ref.[13], page 222, one uses the following value of  $(K\delta)_{sh}$  for 65-series blades,

$$(K\delta)_{sh} = 1.0$$

At this point all the necessary data has been obtained for equations (3) and (4),

$$\delta_o^\circ = (1.0)(0.29)(2.50) = 0.725^\circ$$

From equation (3),

$$\delta = 0.725^\circ + 0.235(6.95^\circ) = 2.36^\circ$$

Finally, equation (2) gives the desired value of  $\beta_2$ ,



$$\beta_2 = 54.93^\circ + 2.36^\circ = 57.29^\circ$$

At this point the relative flow angle for node 57 has been obtained,  $\beta_2 = 57.29^\circ$ . These two values of relative flow angles,  $\beta_1 = 61.88^\circ$  for node 43 and  $\beta_2 = 57.29^\circ$  for node 57, are then read in the program as input data for numerical computation.

This process is repeated at each required blade element section for the proper outlet relative flow angle.



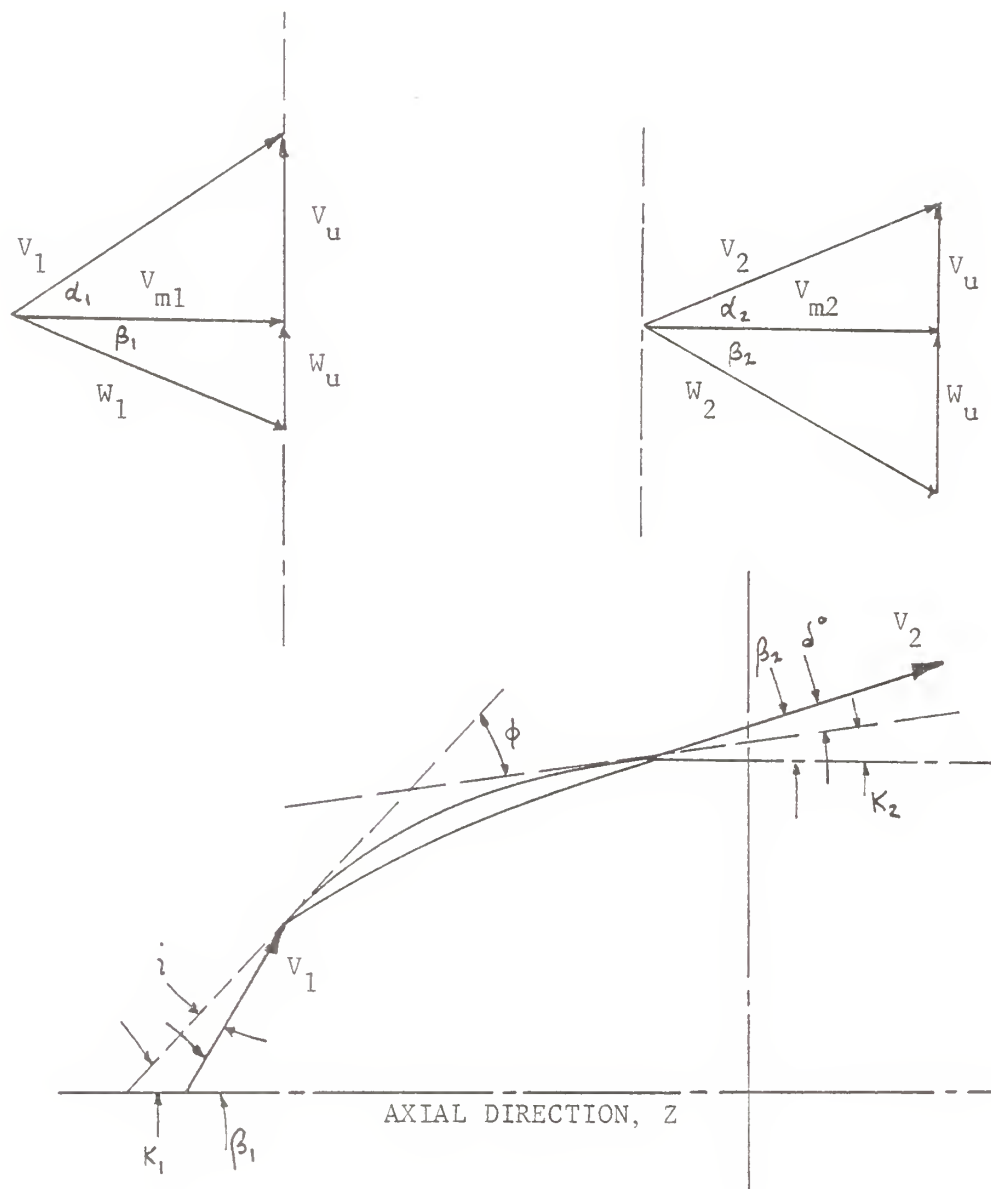


Figure 18 - NOMENCLATURE FOR CASCADE BLADE



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